

MONITORING REPORT

Fourth periodic verification
(version 1, November 26, 2012)

PROJECT: Project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA, company situated in Targu Mures, Romania

Prepared by:



VERTIS FINANCE

Monitoring periods

Line NA2

Project campaign 3
FROM: 14/10/2011
TO: 19/11/2012
ERUs 402,534

Line NA3

Project campaign 3
FROM: 21/07/2011
TO: 07/10/2012
ERUs 786,603

Line NA3

Project campaign 4
FROM: 08/10/2012
TO: 19/11/2012
ERUs 70,519

Line NA4

Project campaign 4
FROM: 15/08/2012
TO: 19/11/2012
ERUs 133,550

Fourth monitoring period start and end: **July 21, 2011 – November 19, 2012**

Fourth monitoring period ERUs in total: **1,393,206**

MONITORING REPORT

PROJECT: Project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA, company situated in Targu Mures, Romania

LINE: Line 2

MONITORING PERIOD:

FROM: 14/10/2011

TO: 19/11/2012

Prepared by:



VERTIS FINANCE

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1. EXECUTIVE SUMMARY

This monitoring report determines baseline emission factor for the Line 2 of Azomures nitric acid plant and quantity of emission reduction generated during the third project campaign on the line.

Total quantity of emission reductions generated during the period from 14/10/2011 through 19/11/2012 on Line 2 is **402 534 ERUs**.

T 1 Emission reduction calculations

EMISSION REDUCTION		
Baseline Emission Factor	EF_BL	11.16 kgN ₂ O/tHNO ₃
Project Campaign Emission Factor	EF_P	1.51 kgN ₂ O/tHNO ₃
Nitric Acid Produced in the Baseline Campaign	NAP_BL	207 983 tHNO ₃
Nitric Acid Produced in the NCSG Baseline Campaign	NAP_BL_NCSG	134 322 tHNO ₃
Nitric Acid Produced in the Project Campaign	NAP_P	134 557 tHNO ₃
GWP	GWP	310 tCO ₂ e/tN ₂ O
Emission Reduction	ER	402 534 tCOe
<i>ER=(EF_BL-EF_P)*NAP_P*GWP/1000</i>		
Abatement Ratio		87.1%

EMISSION REDUCTION PER YEAR			
Year	2010	2011	2012
Date From		14 Oct 2011	01 Jan 2012
Date To		31 Dec 2011	19 Nov 2012
Nitric Acid Production		27 947	106 611
Emission Reduction		83 604	318 930
<i>ER_YR = ER * NAP_P_YR / NAP_P</i>			

Baseline emission factor established for the Line 2 is 11.16 kgN₂O/tHNO₃. The baseline was carried out from 13/07/2007 through 20/10/2008.

The secondary catalyst on Line 2 was installed on 27/10/2008. Project emission factor during the third project campaign, which started on 14/10/2011 and went through 19/11/2012, is 1.51 kgN₂O/tHNO₃.

During the project campaign 134 557 tonnes of nitric acid was produced.

2. DESCRIPTION OF THE PROJECT ACTIVITY

Purpose of the Project (the “Project”) is the reduction of nitrous oxide (N₂O) emissions from Joint Implementation project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA company, situated at Târgu Mures, Romania.

Azomures has installed and operates secondary N₂O reduction catalysts underneath the primary catalyst precious metal catching and catalytic gauzes package in the ammonium burners of all 3 nitric acid plants.

This monitoring report contains information on Line 2 emission reductions including information on baseline emission factor setting for the Line 2.

The separate treatment of the three nitric acid lines and overlapping of the monitoring periods are allowed by the clarification issued Joint Implementation Supervisory Committee: “CLARIFICATION REGARDING OVERLAPPING MONITORING PERIODS UNDER THE VERIFICATION PROCEDURE UNDER THE JOINT IMPLEMENTATION SUPERVISORY COMMITTEE”. The Project meets all the requirement set out by the clarification:

1. The Project is composed of clearly identifiable components for which emission reductions or enhancements of removals are calculated independently; and
2. Monitoring is performed independently for each of these components, i.e. the data/parameters monitored for one component are not dependent on/effect data/parameters (to be) monitored for another component; and
3. The monitoring plan ensures that monitoring is performed for all components and that in these cases all the requirements of the JI guidelines and further guidance by the JISC regarding monitoring are met.

3. BASELINE SETTING

Baseline emission factor for Line 2 has been established on a line-specific basis. Campaign used for baseline measurements on the Line 2 has been carried out from 13/07/2007 through 20/10/2008. Nitric acid production during this campaign did not exceed the historic nitric acid production established as an average production during previous historic campaigns.

N₂O concentration and gas volume flow are monitored by monitoring system complying with requirements of the European Norm 14181.

Monitoring system provides separate readings for N₂O concentration and gas flow volume for every hour of operation as an average of the measured values for the previous 60 minutes.

Measurement results can be distorted before and after periods of downtime or malfunction of the monitoring system and can lead to mavericks. To eliminate such extremes and to ensure a conservative approach, the following statistical evaluation is applied to the complete data series of N₂O concentration as well as to the data series for gas volume flow. The statistical procedure is applied to data obtained after eliminating data measured for periods where the plant operated outside the permitted ranges:

- a) Calculate the sample mean (x)
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG))

The average mass of N₂O emissions per hour is estimated as product of the NCSG and VSG. The N₂O emissions per campaign are estimates product of N₂O emission per hour and the total number of complete hours of operation of the campaign using the following equation:

$$BE_{BC} = VSG_{BC} * NCSG_{BC} * 10^{-9} * OH_{BC} (tN_2O)$$

The line specific baseline emissions factor representing the average N₂O emissions per tonne of nitric acid over one full campaign is derived by dividing the total mass of N₂O emissions by the total output of 100% concentrated nitric acid during baseline campaign.

The overall uncertainty of the monitoring system has been calculated based on the 2008 QAL2 report in its sections 7.5 (also in table 10.5) where separate UNC values for N₂O concentration and tail gas flow are defined. The NA4 QAL2 test report does not contain calculation of total AMS UNC value, only separate UNC values for N₂O concentration and tail gas flow. Total AMS UNC is therefore calculated as $UNC = \sqrt{(2.88^2 + 1.83^2)}$. Total UNC is then 3.41%.

The N₂O emission factor per tonne of nitric acid produced in the baseline period (EFBL) has been then be reduced by the percentage error as follows:

$$EF_{BL} = (BE_{BC} / NAP_{BC}) (1 - UNC/100) (tN_2O/tHNO_3)$$

where:

Variable	Definition
EF_{BL}	Baseline N_2O emissions factor ($tN_2O/tHNO_3$)
BE_{BC}	Total N_2O emissions during the baseline campaign (tN_2O)
$NCSG_{BC}$	Mean concentration of N_2O in the stack gas during the baseline campaign (mgN_2O/m^3)
OH_{BC}	Operating hours of the baseline campaign (h)
VSG_{BC}	Mean gas volume flow rate at the stack in the baseline measurement period (m^3/h)
NAP_{BC}	Nitric acid production during the baseline campaign ($tHNO_3$)
UNC	Overall uncertainty of the monitoring system (%), calculated as the combined uncertainty of the applied monitoring equipment.

3.1 Measurement procedure for N_2O concentration and tail gas volume flow

3.1.1 Tail gas N_2O concentration

- the impulse line is the same as the NO_x outlet line
- the circuit is the same as for measuring NO_x outlet concentration, including up to the pressure reducing valve outlet.
- the gas for the N_2O analyzer is taken from here through a water discharge cooler. The analyzer is produced by Environement S.A., France and is based on non-dispersive infrared absorption principle; it is placed in the same cabinet as the NO_x analyzer. The N_2O concentration measurement range is between 0 – 2000 ppm.
- the outlet analyzer signal is of 4 – 20 mA, proportional to the value of the concentration. This signal is transmitted through an electric cable at the plant's central control panel. The electric cable is approx. 100 m long.
- the device that converts the 4 – 20 mA signal in nitrogen oxides concentration is a ISU – MMC- 24C digital indicator produced by Infostar Pascani. The device has 16 inlet circuits of 4 – 20 mA. The readings are digitally displayed and are recorded every 2 seconds. Data recorded into the "data logger" are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer's hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

3.1.2 Tail gas flow, temperature and pressure

- the measuring point is located on the expansion turbine outlet pipe towards the discharge nozzle; Pytot type sensor with multiple holes; operating conditions: absolute $p = 2.5$ bar, $t = 80^{\circ}\text{C}$

- pneumatic connection line (12 mm diameter and approx. 1 m long hoses) between the sensor and the electric switch box where the Dp cell is located; pneumatic connection line (6 mm diameter and approx. 2 m long hose) between the sensor and the electric switch box where the absolute pressure measuring cell is located

- measuring device: Dp differential transducer, produced by ABB, measuring range between 0 – 30 mbar; absolute pressure transducer produced by Endress&Hauser,

measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C ; analogue output signal 4 – 20 mA

- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA

- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.

- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

3.2 Permitted range of operating conditions of the nitric acid plant

Under certain circumstances, the operating conditions during the measurement period used to determine baseline N_2O emission factor may be outside the permitted range or limit corresponding to normal operating conditions. N_2O baseline data measured during hours where the operating conditions were outside the permitted range have been eliminated from the calculation of the baseline emissions factor.

Normal ranges for operating conditions have been determined for the following parameters:

- oxidation temperature;
- oxidation pressure;
- ammonia gas flow rate,
- air input flow rate.

The permitted range for these parameters has been established using the plant operation manual, as described in the PDD.

3.3 Composition of the ammonia oxidation catalyst

It is business-as-usual in Azomures to change composition of oxidation catalysts installed between campaigns, so the composition during historic and the baseline campaigns is varying.

Reason for switching from Heraeus to Johnson Matthey supplier of primary catalysts for plant NA2 between baseline campaign and third project campaign was of financial nature. Type of the catalyst and its composition (just minor change in the composition caused by slightly different ratio between 3 main precious metal components) remained the same, just the supplier has changed. This change had no impact on N₂O formation underneath the primary catalysts and in the tail gas. Use of this type of primary catalysts is the industry standard.

3.4 Historic Campaign Length

The average historic campaign length (CL_{normal}) defined as the average campaign length for the historic campaigns used to define operating condition (the previous 4 campaigns), has been used as a cap on the length of the baseline campaign.

3.5 Regulatory baseline emissions factor

There are no regulatory limits of N₂O whether defined as mass or concentration limits existent in Romania and there are no limits defined in the Azomures IPPC permit. Project thus uses baseline emission factor as measured during the baseline campaign.

4. PROJECT EMISSIONS

During the third project campaign on Line 2 the tail gas volume flow in the stack of the nitric acid plant as well as N₂O concentration have been measured on a continuous basis.

4.1.1 Estimation of campaign-specific project emissions factor

The monitoring system was installed using the guidance document EN 14181 and provides separate readings for N₂O concentration and gas flow volume for every hour of operation. Same statistical evaluation that was applied to the baseline data series has been applied to the project data series:

- a) Calculate the sample mean (x)
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values

$$PE_n = VSG * NCSG * 10^{-9} * OH \text{ (tN}_2\text{O)}$$

where:

Variable	Definition
VSG	Mean stack gas volume flow rate for the project campaign (m ³ /h)
NCSG	Mean concentration of N ₂ O in the stack gas for the project campaign (mgN ₂ O/m ³)
PE _n	Total N ₂ O emissions of the n th project campaign (tN ₂ O)
OH	Is the number of hours of operation in the specific monitoring period (h)

4.1.2 Derivation of a moving average emission factor

Because the project emission factor measured was lower than the moving average EF of the campaigns on this line so far, we have used the average EF for the calculation of the quantity of emission reductions generated during this campaign.

4.2 Minimum project emission factor

Because this campaign was third project campaign on Line 2 there has been no minimum average emission factor established yet for this campaign. This factor will be established after 10th project campaign.

4.3 Project Campaign Length

Project campaign production of nitric acid 134 557 tHNO₃ was lower than the nameplate capacity of the plant. Project campaign length was shorter than the historic campaign length and also shorter than the baseline campaign length and thus the baseline campaign length in terms of the N₂O concentration measurements has been shortened for calculation of the baseline emission factor and the emission reductions.

4.4 Leakage

No leakage calculation is required.

4.5 Emission reductions

The emission reductions for the project activity during this campaign have been determined by deducting the campaign-specific emission factor from the baseline emission factor and multiplying the result by the production output of 100% concentrated nitric acid over the campaign period and the GWP of N₂O:

$$ER = (EFBL - EFP) * NAP * GWPN_2O \text{ (tCO}_2\text{e)}$$

Where:

Variable	Definition
ER	Emission reductions of the project for the specific campaign (tCO ₂ e)
NAP	Nitric acid production for the project campaign (tHNO ₃). The maximum value of NAP shall not exceed the design capacity.
EFBL	Baseline emissions factor (tN ₂ O/tHNO ₃)
EFP	Emissions factor used to calculate the emissions from this particular campaign (i.e. the higher of EF _{ma,n} and EF _n)

5. MONITORING PLAN

5.1 Main air flow

- the measuring point is located on the compressor air discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 10 m long
- measuring device: Fischer Roesmount differential electronic transducer, having a measuring range between 0 – 45.24 mbar; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 30 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.2 Secondary air flow

- the measuring point is located on the air compressor discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 15 m long

- measuring device: Fischer Roesmount differential electronic transducer, having a measuring range between 0 – 500 mm H₂O; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 50 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.3 Casing protection air flow

- the measuring point is located on the air duct to the reactors casing, ramifications from the compressor discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 10 m long
- measuring device: FEPA Birlad differential electronic transducer, having a measuring range between 0 – 1500 mm H₂O; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 60 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.4 Reactor sieves temperature

- the measuring point is located on the oxidation reactor; sensor; PtRh-Pt thermocouple, operating conditions: $t = 800 - 1000^{\circ}\text{C}$
- electric signal transmission between the sensor and the transducer: PtRh-Pt correction cable, approx. 50 m long
- digital indicator measuring device; measuring range between $0 - 1000^{\circ}\text{C}$; analogue output signal $4 - 20 \text{ mA}$
- signal transmission: electric wires, approx. 6 m long, analogue signal $4 - 20 \text{ mA}$
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.5 Consumed liquid ammonia flow

- the measuring point is located on the ammonia evaporator inlet pipe; Coriolis type sensor; operating conditions: $p = 12 \text{ bar}$, $t = 8 - 10^{\circ}\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 90 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between $0 - 20 \text{ t/h}$; analogue output signal $4 - 20 \text{ mA}$
- signal transmission: electric wires, approx. 10 m long, analogue signal $4 - 20 \text{ mA}$
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.6 Flow of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; electromagnetic sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between 0 – 100 t/h; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.7 Temperature of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; Coriolis type sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between $-50 - 200^\circ\text{C}$; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this

database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.8 Density of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; Coriolis type sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between 1.2 – 1.4 kg/l; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.9 Tail gases flow, tail gases pressure, tail gases temperature

- the measuring point is located on the expansion turbine outlet pipe towards the discharge nozzle; Pytot type sensor with multiple holes; operating conditions: absolute $p = 2.5 \text{ bar}$, $t = 80^\circ\text{C}$
- pneumatic connection line (12 mm diameter and approx. 1 m long hoses) between the sensor and the electric switch box where the Dp cell is located; pneumatic connection line (6 mm diameter and approx. 2 m long hose) between the sensor and the electric switch box where the absolute pressure measuring cell is located
- measuring device: Dp differential transducer, produced by ABB, measuring range between 0 – 30 mbar; absolute pressure transducer produced by Endress&Hauser, measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA

- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.10 Oxidation reactor pressure

- the measuring point is located on the air compressor discharge pipe; sensor type: capsule for electronic transducer; operating conditions: absolute $p = 3.5 \text{ bar}$, $t = 200^\circ\text{C}$
- pneumatic connection line between the sensor and the transducer; pneumatic connection line of 8 mm diameter and approx. 10 m long
- measuring device: Foxboro transducer, measuring range between 0 – 5 bar; absolute pressure transducer produced by Endress&Hauser, measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 50 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.11 N₂O concentration

- the impulse line is the same as the NOx outlet line
- the circuit is the same as for measuring NOx outlet concentration, including up to the pressure reducing valve outlet.
- the gas for the N₂O analyzer is taken from here through a water discharge cooler. The analyzer is produced by Environement S.A., France and is based on non-dispersive infrared

absorption principle; it is placed in the same cabinet as the NOx analyzer. The N2O concentration measurement range is between 0 – 2000 ppm.

- the outlet analyzer signal is of 4 – 20 mA, proportional to the value of the concentration. This signal is transmitted through an electric cable at the plant's central control panel. The electric cable is approx. 100 m long.
- the device that converts the 4 – 20 mA signal in nitrogen oxides concentration is a ISU – MMC- 24C digital indicator produced by Infostar Pascani. The device has 16 inlet circuits of 4 – 20 mA. The readings are digitally displayed and are recorded every 2 seconds. Data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer's hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

6. QAL 2 CALIBRATION ADJUSTMENTS

6.1 Applied principle

As required in the applicable norm EN14181: “The relation between the instrument readings of the recording measuring procedure and the quantity of the measuring objects has to be described by using a suitable convention method. The results have to be expressed by a regression analysis.”

QAL2 test providing regression lines and the combined uncertainty as further used in the model was performed in February 25 28, 2008 by company Airtec holding the ISO 17025 accreditation. During AST tests in August 3 – 6, 2009 and October 28, 2010 done by company SGS holding the ISO 17025 accreditation the NA4 measurements passed the test.

Measurement results derived from the analog signals (4 mA to 20 mA) provided the installed instruments have been compared to the comparative measurements.

Linearity check of the instruments characteristics is stated in the QAL2 Calibration Report issued by the laboratory. The valid ranges of linearity are determined by statistical analysis according to the guideline and the linearity assumptions are further used in the Calibration Report establishing linear regression lines.

The general formula of the regression line, established in the EN14181 and used in the Calibration Report is:

$$Y = a + bX$$

where:

X is the measured value of the instrument in mA
Y is the value of the parameter being objective of the measurement
a is a constant of the regression line
b is the slope of the regression line

After a comparative test the laboratory issued the old and new regression lines properties, namely “a” and “b” applying for all of the measured parameters that are subject to calibration as stated in the Calibration Report.

The QAL2 corrections are based on the fact that the actual analog current outputs (in mA) of the measurement instruments are relevant for both, the old and new regression lines:

$$X_o = X_n = X$$

where :

Xn: X new
Xo: X old

This allows us to derive a calibrating formula that gives us the corrected value of the measured physical parameters. The applied calibrating equation is:

$$Y_n = A_n + (B_n/B_o) * (Y_o - A_o)$$

In order to take into account the properties of the AMS and their implication to the QAL 2 implementation in the model, we will further introduce several remarks to the conversion and normalization of the data.

The units returned by the AMS in “Nm³/h” stand for normalized cubic meters of the gas volume at normal gas conditions (0° C, 1 atm.).

6.2 Stack gas volume flow

The measurement system captures and logs normalized stack volume flow in an integrated manner, calculating the final figure from the mA signal of the endpoints by itself, as opposing to storing just temperature and pressure and deriving the volume flow later. Therefore, the volume flow values can be used as input for QAL2 recalibration transformation without de-normalization and the need for temperature, pressure, and duct cross-section area. The normalized calibrated stack gas flow rates are further fed into the emission calculation model for processing as set out by the Approved Baseline and Monitoring Methodology AM_0034.

6.3 Nitrous oxide concentration in stack gas

The nitric acid concentration in the raw data set from the AMS is in ppm (parts per million). After QAL2 re-calibration, the values are converted to mgN₂O/Nm³ (mg N₂O per normalized cubic meter) to make it fit into the formulas set out in the methodology.

7. EMISSION REDUCTION CALCULATIONS

Table T 2 illustrates the establishment of historic campaign length based on 4 previous campaigns. Average production in campaigns preceding the baseline campaign was 260 782 tHNO₃ and time duration was on average 401 days. Table contains also information on suppliers of primary catalysts for Line 2 (4 burners). As shown in the table, it is usual practice in Azomures to use primary catalysts from two suppliers.

T 2 Historic campaigns

Line	AzoMures-2	Production	Start	End	Days	Production per day	Primary Catalyst	Composition
Historic Campaigns	1 t HNO ₃	-	-	-	-	n/a	N/A	N/A
	2 t HNO ₃	241 277	11 Sep 2001	15 Jun 2003	642	376	Engelhart-Cal	N/A *
	3 t HNO ₃	250 030	19 Jun 2003	01 Aug 2004	409	611	OMG AG	N/A *
	4 t HNO ₃	319 467	20 Aug 2004	14 Feb 2006	543	588	Umicore Degussa	N/A *
	5 t HNO ₃	232 352	03 Apr 2006	21 May 2007	413	563	Umicore Degussa	N/A *
Average HNO₃ production		260 782			401	650	* Confidential, but available for verification	
Project Campaigns	BL t HNO ₃	207 983	13 Jul 2007	20 Oct 2008	465	447	Heraous	N/A *
	PL t HNO ₃	134 557	14 Oct 2011	19 Nov 2012	402	335	Johnson Matthey	N/A *

Table The project campaign production value of 134 557 tHNO₃ was lower than historic nitric acid production set at level of 260 782 tHNO₃.

T 3 and Chart C 1 define the length of the baseline campaign set according to the historic campaign length. Baseline campaign measurements was carried out from 13/07/2007 through 20/10/2008. During baseline campaign, a total of 207 983 tHNO₃ was produced, NCSG measurements are taken into account until the production of 134 322 tHNO₃ was reached.

The project campaign production value of 134 557 tHNO₃ was lower than historic nitric acid production set at level of 260 782 tHNO₃.

T 3 Baseline campaign length

AzoMures-2	Historic Campaigns End	Start of Baseline Measurement	End of Baseline Measurement NCSG	End of Baseline Measurement	End of Baseline Campaign
Dates	2007 May 21	2007 Jul 13	2008 May 07	2008 Oct 20	2008 Oct 21
Baseline Factor kgN ₂ O/tHNO ₃	-	-	11.16	11.16	11.16
Production tHNO ₃	-	-	134 322	207 983	-
Per Day Production tHNO ₃	649.7				
Baseline less Historic Production	(52 799.0)				
Baseline less Historic Days	(81.3)				

C 1 Baseline campaign length

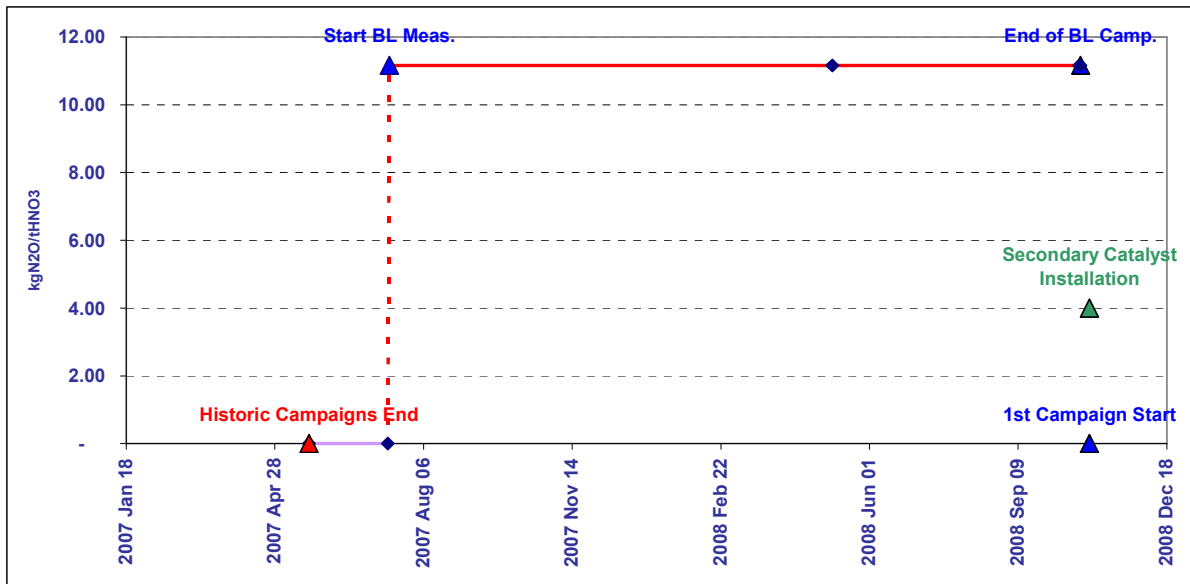


Table T 4 illustrates the calculation of the baseline emission factor on Line 2 using the method as defined in the CDM methodology AM0034 and in the PDD. Baseline measurement was carried out from 13/07/2007 through 20/10/2008.

Extreme values and data measured during hours when one or more of operating conditions were outside of the permitted range have been eliminated from the calculations. As a next step we have eliminated data beyond 95% confidence interval and calculated new mean values of N₂O concentration and stack gas volume flow using following method:

- a) Calculate the sample mean (x)
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG))

Using the means values we have calculated the baseline emissions as set out in the PDD.

$$BE_{BC} = VSG_{BC} * NCSG_{BC} * 10^{-9} * OH_{BC} (tN_2O)$$

Operating hours defined as hours, when nitric acid production at least 0.1 tHNO₃ and oxidation temperature at least 640°C occurred. Calculated baseline N₂O emissions were 1,194 tN₂O.

$$EF_{BL} = (BE_{BC} / NAP_{BC}) (1 - UNC/100) (tN_2O/tHNO_3)$$

The UNC factor defined by the QAL2 report is 3.360%. As a result we have arrived to the baseline emission factor of 11.16 kgN₂O/tHNO₃.

Table T5 shows the calculation of the project emission factor on Line 2 during the project campaign. Project campaign started on 14/10/2011 and went through 19/11/2012.

We have eliminated extreme values and data beyond the 95% confidence interval as prescribed by the PDD.

- a) Calculate the sample mean (\bar{x})
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values

Using the mean values we have calculated total mass of N_2O emissions (PE_n) as follows:

$$PE_n = VSG * NCSG * 10^{-9} * OH (tN_2O)$$

Operating hours (OH) defined as hours, when nitric acid production at least 0.1 tHNO₃ and oxidation temperature at least 640°C occurred.

By dividing total mass of N_2O emissions by the nitric acid production (capped by nameplate capacity 725 tHNO₃/day) we have determined the project campaign specific emission factor at value of 1.51 kgN₂O/tHNO₃.

$$EF_n = PE_n / NAP_n (tN_2O/tHNO_3)$$

This emission factor has been used in further calculation of emission reductions. Neither moving average emission factor nor minimum emission factor was established, since it was the first project campaign.

T 4 Baseline emission factor

BASELINE EMISSION FACTOR									
Parameter	Operating Hours	Nitric Acid Production	N2O Concentration	Gas Volume Flow	Ammonia Flow Rate	Ammonia to Air Ratio	Oxidation Temperature	Oxidation Pressure	
Code Unit	OH h	NAP t/h	NCSG mg N2O/Nm3	VSG Nm3/h	AFR Nm3/h	AIFR %	OT °C	OP kPa	
Elimination of extreme values									
Lower limit	0	0	0	0	0	0	50	0	
Upper limit	60.00	60.00	5.000	200.000	18.000	20.00	1.200	1.000	
Raw Data Measured Range									
Count	8 132	10 112	5 961	10 109	10 100	10 108	10 107	9 299	
as % of Dataset	80%	100%	59%	100%	100%	100%	100%	92%	
Minimum	-	-	3	576	-	0	(26)	-	
Maximum	40.70	40.70	4 321	130 424	16 424	1.37	876	403	
Mean	20.57	20.57	2 481	102 619	9 743	0.16	735	309	
Standard Deviation	9.36	9.36	1 244	31 897	3 817	0.15	280	140	
Total	207 983								
N2O Emissions (VSG * NCSG * OH)									
Emission Factor	2 070	t N2O	9.62	kgN2O / tHNO3					
Permitted Range									
Minimum	7 800	0					800	0	
Maximum	12 000	0.13					880	400	
Data within the permitted range									
Count	5 750	2 987	37%	5 750			71%		
as % of Operating Hours	71%	6		-					
Minimum	4 321	4 321		130 424					
Maximum	2 552	2 552		113 928					
Mean	947	947		8 069					
Standard Deviation									
N2O Emissions (VSG * NCSG * OH)									
Emission Factor	2 364	t N2O	10.98	kgN2O / tHNO3					
Data within the confidence interval									
95% Confidence interval									
Lower bound	695	98 112		129 744					
Upper bound	4 408	4 408		5 726					
Count	2 942	36%		70%					
as % of Operating Hours	1 176	99 844		129 653					
Minimum	4 321	114 289		4 903					
Maximum	2 585	2 585							
Mean	914	914							
Standard Deviation									
N2O Emissions (VSG * NCSG * OH)									
Emission Factor (EF_BL)	2 402	t N2O	11.16	kgN2O / tHNO3					



T 5 Project emission factor

PROJECT EMISSION FACTOR									
Parameter	Operating Hours	Nitric Acid Production	N2O Concentration	Gas Volume Flow	Ammonia Flow Rate	Ammonia to Air Ratio	Oxidation Temperature	Oxidation Pressure	
Code Unit	OH h	NAP t/h	NCSG mg N2O/Nm3	VSG Nm3/h	AFR Nm3/h	AIFR %	OT °C	OP kPa	
Elimination of extreme values									
Lower limit		0	0	0	0	0	-	50	0
Upper Limit	60.00	60.00	5.000	200 000	18 000	20.00	1 200	1 000	1 000
Raw Data Measured Range									
Count	5 797	9 531	7 513	9 532	6 17	6 556	9 532	6 595	
as % of Dataset	61%	100%	79%	100%	6%	69%	100%	69%	
Minimum	-	-	0	-	-	0	(31)	-	
Maximum	29.73	29.73	1 359	115 825	12 521	19.89	858	410	
Mean	14.12	14.12	262	70 018	2 183	0.31	258	325	
Standard Deviation	11.41	11.41	185	42 862	4 459	1.24	403	117	
Total	134 557								
N2O Emissions (VSG * NCSG * OH)									
N2O Emission Factor	106 t N2O	0.79 kgN2O / tHNO3							
Data within the confidence interval									
95% Confidence interval									
Lower bound	-	-	100	-	13 991				
Upper bound			624	154 027					
Count			5 660	5 787					
as % of Operating Hours			98%	100%					
Minimum			0	12 925					
Maximum			610	115 825					
Mean			321	103 779					
Standard Deviation			96	5 869					
N2O Emissions (VSG * NCSG * OH)									
N2O Emissions (VSG * NCSG * OH)	193 t N2O								
Actual Project Emission Factor (EF_P Actual)	1.44 kgN2O / tHNO3								
Abatement Ratio	87.1%								
Moving Average Emission Factor Correction									
	Actual Factors	Moving Average Rule							
1	0.93	0.93							
2	2.17	2.17							
3	1.44	1.51							
4	-	-							
Project Emission Factor (EF_P)									
Project Emission Factor (EF_P)	1.51 kgN2O / tHNO3								
Abatement Ratio	86.5%								

MONITORING REPORT

PROJECT: Project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA, company situated in Targu Mures, Romania

LINE: Line 3

MONITORING PERIOD:

FROM: 21/07/2011

TO: 07/10/2012

Prepared by:



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1. EXECUTIVE SUMMARY

This monitoring report determines baseline emission factor for the Line 3 of Azomures nitric acid plant and quantity of emission reduction generated during the third project campaign on the line.

Total quantity of emission reductions generated during the period from 21/07/2011 through 07/10/2012 on Line 3 is **786 603 ERUs**.

T 1 Emission reduction calculations

EMISSION REDUCTION		
Baseline Emission Factor	EF_BL	12.32 kgN ₂ O/tHNO ₃
Project Campaign Emission Factor	EF_P	2.13 kgN ₂ O/tHNO ₃
Nitric Acid Produced in the Baseline Campaign	NAP_BL	215 669 tHNO ₃
Nitric Acid Produced in the NCSG Baseline Campaign	NAP_BL_NCSG	215 669 tHNO ₃
Nitric Acid Produced in the Project Campaign	NAP_P	248 868 tHNO ₃
GWP	GWP	310 tCO ₂ e/tN ₂ O
Emission Reduction	ER	786 603 tCO₂e
<i>ER=(EF_BL-EF_P)*NAP_P*GWP/1000</i>		
Abatement Ratio		83.9%

EMISSION REDUCTION PER YEAR			
Year	2010	2011	2012
Date From		21 Jul 2011	01 Jan 2012
Date To		31 Dec 2011	07 Oct 2012
Nitric Acid Production		118 646	130 222
Emission Reduction		375 007	411 596
<i>ER_YR = ER * NAP_P_YR / NAP_P</i>			

Baseline emission factor established for the Line 3 is 12.32 kgN₂O/tHNO₃. The baseline was carried out from 02/03/2007 through 14/07/2008.

The secondary catalyst on Line 3 was installed on 18/07/2008. Project emission factor during the third project campaign, which started on 21/07/2011 and went through 07/10/2012, is 2.13 kgN₂O/tHNO₃.

During the project campaign 248 868 tonnes of nitric acid was produced.

2. DESCRIPTION OF THE PROJECT ACTIVITY

Purpose of the Project (the “Project”) is the reduction of nitrous oxide (N₂O) emissions from Joint Implementation project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA company, situated at Târgu Mures, Romania.

Azomures has installed and operates secondary N₂O reduction catalysts underneath the primary catalyst precious metal catching and catalytic gauzes package in the ammonium burners of all 3 nitric acid plants.

This monitoring report contains information on Line 3 emission reductions including information on baseline emission factor setting for the Line 3.

The separate treatment of the three nitric acid lines and overlapping of the monitoring periods are allowed by the clarification issued Joint Implementation Supervisory Committee: “CLARIFICATION REGARDING OVERLAPPING MONITORING PERIODS UNDER THE VERIFICATION PROCEDURE UNDER THE JOINT IMPLEMENTATION SUPERVISORY COMMITTEE”. The Project meets all the requirement set out by the clarification:

1. The Project is composed of clearly identifiable components for which emission reductions or enhancements of removals are calculated independently; and
2. Monitoring is performed independently for each of these components, i.e. the data/parameters monitored for one component are not dependent on/effect data/parameters (to be) monitored for another component; and
3. The monitoring plan ensures that monitoring is performed for all components and that in these cases all the requirements of the JI guidelines and further guidance by the JISC regarding monitoring are met.

3. BASELINE SETTING

Baseline emission factor for Line 3 has been established on a line-specific basis. Campaign used for baseline measurements on the Line 3 has been carried out from 02/03/2007 through 14/07/2008. Nitric acid production during this campaign did not exceed the historic nitric acid production established as an average production during previous historic campaigns.

N₂O concentration and gas volume flow are monitored by monitoring system complying with requirements of the European Norm 14181.

Monitoring system provides separate readings for N₂O concentration and gas flow volume for every hour of operation as an average of the measured values for the previous 60 minutes.

Measurement results can be distorted before and after periods of downtime or malfunction of the monitoring system and can lead to mavericks. To eliminate such extremes and to ensure a conservative approach, the following statistical evaluation is applied to the complete data series of N₂O concentration as well as to the data series for gas volume flow. The statistical procedure is applied to data obtained after eliminating data measured for periods where the plant operated outside the permitted ranges:

- a) Calculate the sample mean (x)
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG))

The average mass of N₂O emissions per hour is estimated as product of the NCSG and VSG. The N₂O emissions per campaign are estimates product of N₂O emission per hour and the total number of complete hours of operation of the campaign using the following equation:

$$BE_{BC} = VSG_{BC} * NCSG_{BC} * 10^{-9} * OH_{BC} (tN_2O)$$

The line specific baseline emissions factor representing the average N₂O emissions per tonne of nitric acid over one full campaign is derived by dividing the total mass of N₂O emissions by the total output of 100% concentrated nitric acid during baseline campaign.

The overall uncertainty of the monitoring system has been calculated based on the 2008 QAL2 report in its sections 7.5 (also in table 10.5) where separate UNC values for N₂O concentration and tail gas flow are defined. The NA4 QAL2 test report does not contain calculation of total AMS UNC value, only separate UNC values for N₂O concentration and tail gas flow. Total AMS UNC is therefore calculated as $UNC = \sqrt{(2.88^2 + 1.83^2)}$. Total UNC is then 3.41%.

The N₂O emission factor per tonne of nitric acid produced in the baseline period (EFBL) has been then be reduced by the percentage error as follows:

$$EF_{BL} = (BE_{BC} / NAP_{BC}) (1 - UNC/100) (tN_2O/tHNO_3)$$

where:

Variable	Definition
EF_{BL}	Baseline N_2O emissions factor ($tN_2O/tHNO_3$)
BE_{BC}	Total N_2O emissions during the baseline campaign (tN_2O)
$NCSG_{BC}$	Mean concentration of N_2O in the stack gas during the baseline campaign (mgN_2O/m^3)
OH_{BC}	Operating hours of the baseline campaign (h)
VSG_{BC}	Mean gas volume flow rate at the stack in the baseline measurement period (m^3/h)
NAP_{BC}	Nitric acid production during the baseline campaign ($tHNO_3$)
UNC	Overall uncertainty of the monitoring system (%), calculated as the combined uncertainty of the applied monitoring equipment.

3.1 Measurement procedure for N_2O concentration and tail gas volume flow

3.1.1 Tail gas N_2O concentration

- the impulse line is the same as the NO_x outlet line
- the circuit is the same as for measuring NO_x outlet concentration, including up to the pressure reducing valve outlet.
- the gas for the N_2O analyzer is taken from here through a water discharge cooler. The analyzer is produced by Environement S.A., France and is based on non-dispersive infrared absorption principle; it is placed in the same cabinet as the NO_x analyzer. The N_2O concentration measurement range is between 0 – 2000 ppm.
- the outlet analyzer signal is of 4 – 20 mA, proportional to the value of the concentration. This signal is transmitted through an electric cable at the plant's central control panel. The electric cable is approx. 100 m long.
- the device that converts the 4 – 20 mA signal in nitrogen oxides concentration is a ISU – MMC- 24C digital indicator produced by Infostar Pascani. The device has 16 inlet circuits of 4 – 20 mA. The readings are digitally displayed and are recorded every 2 seconds. Data recorded into the "data logger" are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer's hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

3.1.2 Tail gas flow, temperature and pressure

- the measuring point is located on the expansion turbine outlet pipe towards the discharge nozzle; Pytot type sensor with multiple holes; operating conditions: absolute $p = 2.5$ bar, $t = 80^{\circ}\text{C}$

- pneumatic connection line (12 mm diameter and approx. 1 m long hoses) between the sensor and the electric switch box where the Dp cell is located; pneumatic connection line (6 mm diameter and approx. 2 m long hose) between the sensor and the electric switch box where the absolute pressure measuring cell is located

- measuring device: Dp differential transducer, produced by ABB, measuring range between 0 – 30 mbar; absolute pressure transducer produced by Endress&Hauser,

measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C ; analogue output signal 4 – 20 mA

- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA

- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.

- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

3.2 Permitted range of operating conditions of the nitric acid plant

Under certain circumstances, the operating conditions during the measurement period used to determine baseline N_2O emission factor may be outside the permitted range or limit corresponding to normal operating conditions. N_2O baseline data measured during hours where the operating conditions were outside the permitted range have been eliminated from the calculation of the baseline emissions factor.

Normal ranges for operating conditions have been determined for the following parameters:

- oxidation temperature;
- oxidation pressure;
- ammonia gas flow rate,
- air input flow rate.

The permitted range for these parameters has been established using the plant operation manual, as described in the PDD.

3.3 Composition of the ammonia oxidation catalyst

Supplier of primary catalysts for plant NA3 between baseline campaign and third project campaign remained same as well as its composition.

3.4 Historic Campaign Length

The average historic campaign length (CL_{normal}) defined as the average campaign length for the historic campaigns used to define operating condition (the previous 4 campaigns), has been used as a cap on the length of the baseline campaign.

3.5 Regulatory baseline emissions factor

There are no regulatory limits of N₂O whether defined as mass or concentration limits existent in Romania and there are no limits defined in the Azomures IPPC permit. Project thus uses baseline emission factor as measured during the baseline campaign.

4. PROJECT EMISSIONS

During the third project campaign on Line 3 the tail gas volume flow in the stack of the nitric acid plant as well as N₂O concentration have been measured on a continuous basis.

4.1.1 Estimation of campaign-specific project emissions factor

The monitoring system was installed using the guidance document EN 14181 and provides separate readings for N₂O concentration and gas flow volume for every hour of operation. Same statistical evaluation that was applied to the baseline data series has been applied to the project data series:

- a) Calculate the sample mean (\bar{x})
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values

$$PE_n = VSG * NCSG * 10^{-9} * OH \text{ (tN}_2\text{O)}$$

where:

Variable	Definition
VSG	Mean stack gas volume flow rate for the project campaign (m ³ /h)
NCSG	Mean concentration of N ₂ O in the stack gas for the project campaign (mgN ₂ O/m ³)
PE _n	Total N ₂ O emissions of the n th project campaign (tN ₂ O)
OH	Is the number of hours of operation in the specific monitoring period (h)

4.1.2 Derivation of a moving average emission factor

Because the project emission factor measured was lower than the moving average EF of the campaigns on this line so far, we have used the average EF for the calculation of the quantity of emission reductions generated during this campaign.

4.2 Minimum project emission factor

Because this campaign was third project campaign on Line 3 there has been no minimum average emission factor established yet for this campaign. This factor will be established after 10th project campaign.

4.3 Project Campaign Length

Project campaign length was longer than the campaign length normal and thus all N₂O values measured during the project campaign were used for calculation of the emission factor.

4.4 Leakage

No leakage calculation is required.

4.5 Emission reductions

The emission reductions for the project activity during this campaign have been determined by deducting the campaign-specific emission factor from the baseline emission factor and multiplying the result by the production output of 100% concentrated nitric acid over the campaign period and the GWP of N₂O:

$$ER = (EFBL - EFP) * NAP * GWPN_2O \text{ (tCO}_2\text{e)}$$

Where:

Variable	Definition
ER	Emission reductions of the project for the specific campaign (tCO ₂ e)
NAP	Nitric acid production for the project campaign (tHNO ₃). The maximum value of NAP shall not exceed the design capacity.
EFBL	Baseline emissions factor (tN ₂ O/tHNO ₃)
EFP	Emissions factor used to calculate the emissions from this particular campaign (i.e. the higher of EF _{ma,n} and EF _n)

5. MONITORING PLAN

5.1 Main air flow

- the measuring point is located on the compressor air discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 10 m long
- measuring device: Fischer Roesmount differential electronic transducer, having a measuring range between 0 – 45.24 mbar; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 30 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.2 Secondary air flow

- the measuring point is located on the air compressor discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 15 m long

- measuring device: Fischer Roesmount differential electronic transducer, having a measuring range between 0 – 500 mm H₂O; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 50 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.3 Casing protection air flow

- the measuring point is located on the air duct to the reactors casing, ramifications from the compressor discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 10 m long
- measuring device: FEPA Birlad differential electronic transducer, having a measuring range between 0 – 1500 mm H₂O; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 60 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.4 Reactor sieves temperature

- the measuring point is located on the oxidation reactor; sensor; PtRh-Pt thermocouple, operating conditions: $t = 800 - 1000^{\circ}\text{C}$
- electric signal transmission between the sensor and the transducer: PtRh-Pt correction cable, approx. 50 m long
- digital indicator measuring device; measuring range between $0 - 1000^{\circ}\text{C}$; analogue output signal $4 - 20 \text{ mA}$
- signal transmission: electric wires, approx. 6 m long, analogue signal $4 - 20 \text{ mA}$
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.5 Consumed liquid ammonia flow

- the measuring point is located on the ammonia evaporator inlet pipe; Coriolis type sensor; operating conditions: $p = 12 \text{ bar}$, $t = 8 - 10^{\circ}\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 90 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between $0 - 20 \text{ t/h}$; analogue output signal $4 - 20 \text{ mA}$
- signal transmission: electric wires, approx. 10 m long, analogue signal $4 - 20 \text{ mA}$
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.6 Flow of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; electromagnetic sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between 0 – 100 t/h; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.7 Temperature of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; Coriolis type sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between $-50 - 200^\circ\text{C}$; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this

database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.8 Density of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; Coriolis type sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between 1.2 – 1.4 kg/l; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.9 Tail gases flow, tail gases pressure, tail gases temperature

- the measuring point is located on the expansion turbine outlet pipe towards the discharge nozzle; Pytot type sensor with multiple holes; operating conditions: absolute $p = 2.5 \text{ bar}$, $t = 80^\circ\text{C}$
- pneumatic connection line (12 mm diameter and approx. 1 m long hoses) between the sensor and the electric switch box where the Dp cell is located; pneumatic connection line (6 mm diameter and approx. 2 m long hose) between the sensor and the electric switch box where the absolute pressure measuring cell is located
- measuring device: Dp differential transducer, produced by ABB, measuring range between 0 – 30 mbar; absolute pressure transducer produced by Endress&Hauser, measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA

- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.10 Oxidation reactor pressure

- the measuring point is located on the air compressor discharge pipe; sensor type: capsule for electronic transducer; operating conditions: absolute $p = 3.5$ bar, $t = 200^{\circ}\text{C}$
- pneumatic connection line between the sensor and the transducer; pneumatic connection line of 8 mm diameter and approx. 10 m long
- measuring device: Foxboro transducer, measuring range between 0 – 5 bar; absolute pressure transducer produced by Endress&Hauser, measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C ; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 50 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.11 N₂O concentration

- the impulse line is the same as the NO_x outlet line
- the circuit is the same as for measuring NO_x outlet concentration, including up to the pressure reducing valve outlet.
- the gas for the N₂O analyzer is taken from here through a water discharge cooler. The analyzer is produced by Environement S.A., France and is based on non-dispersive infrared

absorption principle; it is placed in the same cabinet as the NOx analyzer. The N2O concentration measurement range is between 0 – 2000 ppm.

- the outlet analyzer signal is of 4 – 20 mA, proportional to the value of the concentration. This signal is transmitted through an electric cable at the plant's central control panel. The electric cable is approx. 100 m long.
- the device that converts the 4 – 20 mA signal in nitrogen oxides concentration is a ISU – MMC- 24C digital indicator produced by Infostar Pascani. The device has 16 inlet circuits of 4 – 20 mA. The readings are digitally displayed and are recorded every 2 seconds. Data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer's hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

6. QAL 2 CALIBRATION ADJUSTMENTS

6.1 Applied principle

As required in the applicable norm EN14181: “The relation between the instrument readings of the recording measuring procedure and the quantity of the measuring objects has to be described by using a suitable convention method. The results have to be expressed by a regression analysis.”

QAL2 test providing regression lines and the combined uncertainty as further used in the model was performed in February 25 28, 2008 by company Airtec holding the ISO 17025 accreditation. During AST tests in August 3 – 6, 2009 and October 28, 2010 done by company SGS holding the ISO 17025 accreditation the NA4 measurements passed the test.

Measurement results derived from the analog signals (4 mA to 20 mA) provided the installed instruments have been compared to the comparative measurements.

Linearity check of the instruments characteristics is stated in the QAL2 Calibration Report issued by the laboratory. The valid ranges of linearity are determined by statistical analysis according to the guideline and the linearity assumptions are further used in the Calibration Report establishing linear regression lines.

The general formula of the regression line, established in the EN14181 and used in the Calibration Report is:

$$Y = a + bX$$

where:

X is the measured value of the instrument in mA
Y is the value of the parameter being objective of the measurement
a is a constant of the regression line
b is the slope of the regression line

After a comparative test the laboratory issued the old and new regression lines properties, namely “a” and “b” applying for all of the measured parameters that are subject to calibration as stated in the Calibration Report.

The QAL2 corrections are based on the fact that the actual analog current outputs (in mA) of the measurement instruments are relevant for both, the old and new regression lines:

$$X_o = X_n = X$$

where :

Xn: X new
Xo: X old

This allows us to derive a calibrating formula that gives us the corrected value of the measured physical parameters. The applied calibrating equation is:

$$Y_n = A_n + (B_n/B_o) * (Y_o - A_o)$$

In order to take into account the properties of the AMS and their implication to the QAL 2 implementation in the model, we will further introduce several remarks to the conversion and normalization of the data.

The units returned by the AMS in “Nm³/h” stand for normalized cubic meters of the gas volume at normal gas conditions (0° C, 1 atm.).

6.2 Stack gas volume flow

The measurement system captures and logs normalized stack volume flow in an integrated manner, calculating the final figure from the mA signal of the endpoints by itself, as opposing to storing just temperature and pressure and deriving the volume flow later. Therefore, the volume flow values can be used as input for QAL2 recalibration transformation without de-normalization and the need for temperature, pressure, and duct cross-section area. The normalized calibrated stack gas flow rates are further fed into the emission calculation model for processing as set out by the Approved Baseline and Monitoring Methodology AM_0034.

6.3 Nitrous oxide concentration in stack gas

The nitric acid concentration in the raw data set from the AMS is in ppm (parts per million). After QAL2 re-calibration, the values are converted to mgN₂O/Nm³ (mg N₂O per normalized cubic meter) to make it fit into the formulas set out in the methodology.

7. EMISSION REDUCTION CALCULATIONS

Table T 2 illustrates the establishment of historic campaign length based on 4 previous campaigns. Average production in campaigns preceding the baseline campaign was 286 940 tHNO₃ and time duration was on average 383 days. Table contains also information on suppliers of primary catalysts for Line 3 (4 burners). As shown in the table, it is usual practice in Azomures to use primary catalysts from two suppliers.

T 2 Historic campaigns

Line	AzoMures-3	Production	Start	End	Days	Production per day	Primary Catalyst	Composition
Historic Campaigns	1 t HNO ₃	-	-	-	-	n/a		0 N/A
	2 t HNO ₃	210 275	12 Oct 2001	27 Oct 2002	380	553	Engelhart-Cal	N/A *
	3 t HNO ₃	325 002	08 Nov 2002	13 Apr 2004	522	623	Engelhart-Cal	N/A *
	4 t HNO ₃	349 459	20 Apr 2004	02 Oct 2005	530	659	Engelhart-Cal	N/A *
	5 t HNO ₃	263 025	19 Oct 2005	16 Feb 2007	485	542	Johnson Matthey	N/A *
Average HNO₃ production		286 940			383	748	* Confidential, but available for verification	
Project Campaigns	BL t HNO ₃	215 669	02 Mar 2007	14 Jul 2008	500	432	Johnson Matthey	N/A *
	PL t HNO ₃	248 868	21 Jul 2011	07 Oct 2012	445	559	Johnson Matthey	N/A *

Table The project campaign production value of 248 868 tHNO₃ was lower than historic nitric acid production set at level of 286 940 tHNO₃.

T 3 and Chart C 1 define the length of the baseline campaign set according to the historic campaign length. Baseline campaign measurements was carried out from 02/03/2007 through 14/07/2008. During baseline campaign, a total of 215 669 tHNO₃ was produced, NCSG measurements are taken into account until the production of 215 669 tHNO₃ was reached.

The project campaign production value of 248 868 tHNO₃ was lower than historic nitric acid production set at level of 286 940 tHNO₃.

T 3 Baseline campaign length

AzoMures-3	Historic Campaigns End	Start of Baseline Measurement	End of Baseline Measurement NCSG	End of Baseline Measurement	End of Baseline Campaign
Dates	2007 Feb 16	2007 Mar 02	2008 Jul 14	2008 Jul 14	2008 Jul 15
Baseline Factor kgN ₂ O/tHNO ₃	-	-	12.32	12.32	12.32
Production tHNO ₃	-	-	215 669	215 669	-
Per Day Production tHNO ₃	748.4				
Baseline less Historic Production	(71 271.0)				
Baseline less Historic Days	(95.2)				

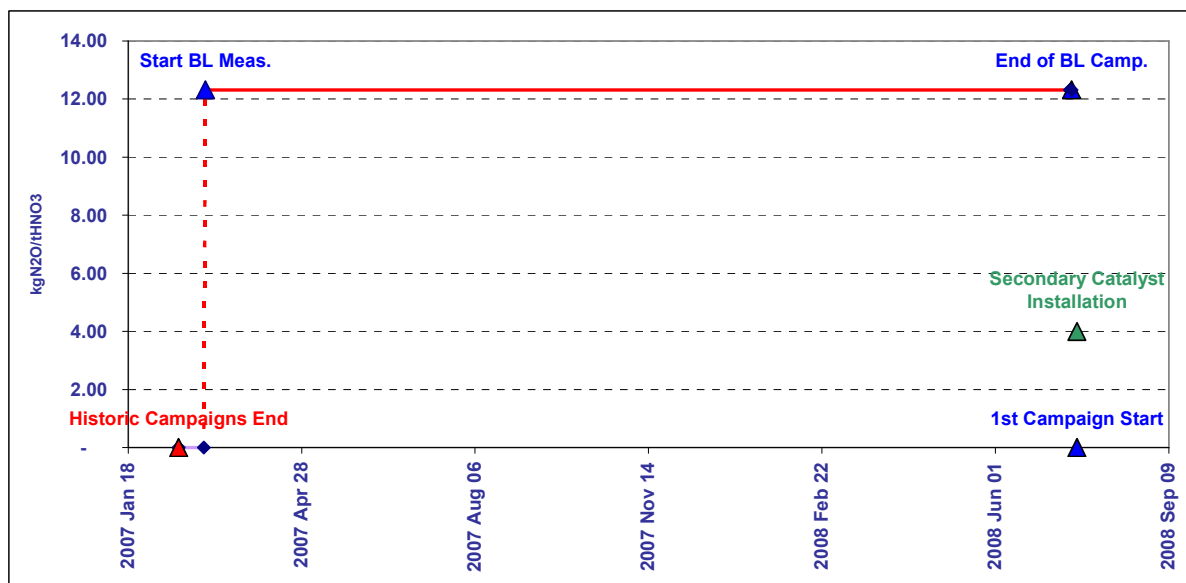
C 1 Baseline campaign length


Table T 4 illustrates the calculation of the baseline emission factor on Line 3 using the method as defined in the CDM methodology AM0034 and in the PDD. Baseline measurement was carried out from 02/03/2007 through 14/07/2008.

Extreme values and data measured during hours when one or more of operating conditions were outside of the permitted range have been eliminated from the calculations. As a next step we have eliminated data beyond 95% confidence interval and calculated new mean values of N₂O concentration and stack gas volume flow using following method:

- Calculate the sample mean (x)
- Calculate the sample standard deviation (s)
- Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- Eliminate all data that lie outside the 95% confidence interval
- Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG))

Using the means values we have calculated the baseline emissions as set out in the PDD.

$$BE_{BC} = VSG_{BC} * NCSG_{BC} * 10^{-9} * OH_{BC} (tN_2O)$$

Operating hours defined as hours, when nitric acid production at least 0.1 tHNO₃ and oxidation temperature at least 640°C occurred. Calculated baseline N₂O emissions were 1,194 tN₂O.

$$EF_{BL} = (BE_{BC} / NAP_{BC}) (1 - UNC/100) (tN_2O/tHNO_3)$$

The UNC factor defined by the QAL2 report is 3.185%. As a result we have arrived to the baseline emission factor of 12.32 kgN₂O/tHNO₃.

Table T5 shows the calculation of the project emission factor on Line 3 during the project campaign. Project campaign started on 21/07/2011 and went through 07/10/2012.

We have eliminated extreme values and data beyond the 95% confidence interval as prescribed by the PDD.

- a) Calculate the sample mean (\bar{x})
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values

Using the mean values we have calculated total mass of N_2O emissions (PE_n) as follows:

$$PE_n = VSG * NCSG * 10^{-9} * OH (tN_2O)$$

Operating hours (OH) defined as hours, when nitric acid production at least 0.1 tHNO₃ and oxidation temperature at least 640°C occurred.

By dividing total mass of N_2O emissions by the nitric acid production (capped by nameplate capacity 725 tHNO₃/day) we have determined the project campaign specific emission factor at value of 2.13 kgN₂O/tHNO₃.

$$EF_n = PE_n / NAP_n (tN_2O/tHNO_3)$$

This emission factor has been used in further calculation of emission reductions. Neither moving average emission factor nor minimum emission factor was established, since it was the first project campaign.

T 4 Baseline emission factor

BASELINE EMISSION FACTOR									
Parameter	Operating Hours	Nitric Acid Production	N2O Concentration	Gas Volume Flow	Ammonia Flow Rate	Ammonia to Air Ratio	Oxidation Temperature	Oxidation Pressure	
Code Unit	OH h	NAP t/h	NCSG mg N2O/Nm3	VSG Nm3/h	AFR Nm3/h	AIFR %	OT °C	OP kPa	
Elimination of extreme values									
Lower limit	0	60.00	5.000	20.000	18.000	0	-	50	0
Upper limit						20.000	1.200	1.000	
Raw Data Measured Range									
Count	8 624	7 388	6 243	6 482	11 915	11 174	11 989	11 431	
as % of Dataset	72%	62%	52%	54%	99%	93%	100%	95%	
Minimum	0.10	0.10	161	20 263	-	-	(31)	-	
Maximum	40.54	40.54	4 321	136 304	15 445	19.94	864	400	
Mean	29.19	29.19	3 902	95 572	7 882	8.53	623	104	
Standard Deviation	4.80	4.80	462	15 376	4 881	4.22	356	117	
Total		215 669							
N2O Emissions (VSG * NCSG * OH)									
Emission Factor									
3 216 tN2O									
14.44 kgN2O / tHNO3									
Permitted Range									
Minimum					8 000	0	800	0	
Maximum					12 500	11.50	860	260	
Data within the permitted range									
Count	8 291		6 877	6 924					
as % of Operating Hours	96%		80%	80%					
Minimum			271	-					
Maximum			4 321	415 934					
Mean			3 286	93 138					
Standard Deviation			1 163	21 931					
N2O Emissions (VSG * NCSG * OH)									
Emission Factor									
2 640 tN2O									
11.85 kgN2O / tHNO3									
Data within the confidence interval									
95% Confidence interval									
Lower bound			1 007	50 153					
Upper bound			5 565	136 122					
Count			6 636	6 468					
as % of Operating Hours			77%	75%					
Minimum			1 028	50 192					
Maximum			4 321	135 386					
Mean			3 374	94 322					
Standard Deviation			1 086	14 628					
N2O Emissions (VSG * NCSG * OH)									
Emission Factor (EF_BL)									
2 745 tN2O									
12.32 kgN2O / tHNO3									



T 5 Project emission factor

PROJECT EMISSION FACTOR									
Parameter	Operating Hours	Nitric Acid Production	N2O Concentration	Gas Volume Flow	Ammonia Flow Rate	Ammonia to Air Ratio	Oxidation Temperature	Oxidation Pressure	
Code Unit	OH h	NAP t/h	NCSG mg N2O/Nm3	VSG Nm3/h	AFR Nm3/h	AIFR %	OT °C	OP kPa	
Elimination of extreme values									
Lower limit	0	60.00	100	20 000	0	0	50	0	
Upper Limit			5 000	200 000	18 000	20.00	1 200	1 000	
Raw Data Measured Range									
Count	8 307	8 830	8 305	8 353	10 678	9 640	10 678	10 128	
as % of Dataset	78%	83%	78%	78%	100%	90%	100%	95%	
Minimum		0.10	100	21 721	-	-	(31)	-	
Maximum		46.04	3 341	125 003	12 934	18.80	862	268	
Mean		28.18	520	112 796	9 014	9.32	392	199	
Standard Deviation		11.55	191	8 354	4 835	3.53	429	93	
Total		248 868							
N2O Emissions (VSG * NCSG * OH)									
N2O Emission Factor	487	t N2O	1.96	kgN2O / tHNO3					
Data within the confidence interval									
95% Confidence interval									
Lower bound				145				96 423	
Upper bound				895				129 170	
Count				8 076				7 980	
as % of Operating Hours				97%				96%	
Minimum				163				96 431	
Maximum				895				125 003	
Mean				522				113 762	
Standard Deviation				184				4 768	
N2O Emissions (VSG * NCSG * OH)									
Actual Project Emission Factor (EF_P Actual)	493	t N2O	1.98	kgN2O / tHNO3					
Abatement Ratio				83.9%					
Moving Average Emission Factor Correction									
	Actual Factors	Moving Average Rule							
1	1.45	1.45							
2	2.94	2.94							
3	1.98	2.13							
4	-	-							
Project Emission Factor (EF_P)									
Abatement Ratio				2.13				kgN2O / tHNO3	
				82.8%					

MONITORING REPORT

PROJECT: Project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA, company situated in Targu Mures, Romania

LINE: Line 3

MONITORING PERIOD:

FROM: 08/10/2012

TO: 19/11/2012

Prepared by:



VERTIS FINANCE

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1. EXECUTIVE SUMMARY

This monitoring report determines baseline emission factor for the Line 3 of Azomures nitric acid plant and quantity of emission reduction generated during the fourth project campaign on the line.

Total quantity of emission reductions generated during the period from 08/10/2012 through 19/11/2012 on Line 3 is **70 519 ERUs**.

T 1 Emission reduction calculations

EMISSION REDUCTION		
Baseline Emission Factor	EF_BL	9.40 kgN ₂ O/tHNO ₃
Project Campaign Emission Factor	EF_P	1.95 kgN ₂ O/tHNO ₃
Nitric Acid Produced in the Baseline Campaign	NAP_BL	215 669 tHNO ₃
Nitric Acid Produced in the NCSG Baseline Campaign	NAP_BL_NCSG	30 097 tHNO ₃
Nitric Acid Produced in the Project Campaign	NAP_P	30 571 tHNO ₃
GWP	GWP	310 tCO ₂ e/tN ₂ O
Emission Reduction	ER	70 519 tCOe
<i>ER=(EF_BL-EF_P)*NAP_P*GWP/1000</i>		
Abatement Ratio		84.6%

EMISSION REDUCTION PER YEAR			
Year	2010	2011	2012
Date From			08 Oct 2012
Date To			19 Nov 2012
Nitric Acid Production			30 571
Emission Reduction			70 519
<i>ER_YR = ER * NAP_P_YR / NAP_P</i>			

Baseline emission factor established for the Line 3 is 9.40 kgN₂O/tHNO₃. The baseline was carried out from 02/03/2007 through 14/07/2008.

The secondary catalyst on Line 3 was installed on 18/07/2008. Project emission factor during the fourth project campaign, which started on 08/10/2012 and went through 19/11/2012, is 1.95 kgN₂O/tHNO₃.

During the project campaign 30 571 tonnes of nitric acid was produced.

2. DESCRIPTION OF THE PROJECT ACTIVITY

Purpose of the Project (the “Project”) is the reduction of nitrous oxide (N₂O) emissions from Joint Implementation project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA company, situated at Târgu Mures, Romania.

Azomures has installed and operates secondary N₂O reduction catalysts underneath the primary catalyst precious metal catching and catalytic gauzes package in the ammonium burners of all 3 nitric acid plants.

This monitoring report contains information on Line 3 emission reductions including information on baseline emission factor setting for the Line 3.

The separate treatment of the three nitric acid lines and overlapping of the monitoring periods are allowed by the clarification issued Joint Implementation Supervisory Committee: “CLARIFICATION REGARDING OVERLAPPING MONITORING PERIODS UNDER THE VERIFICATION PROCEDURE UNDER THE JOINT IMPLEMENTATION SUPERVISORY COMMITTEE”. The Project meets all the requirement set out by the clarification:

1. The Project is composed of clearly identifiable components for which emission reductions or enhancements of removals are calculated independently; and
2. Monitoring is performed independently for each of these components, i.e. the data/parameters monitored for one component are not dependent on/effect data/parameters (to be) monitored for another component; and
3. The monitoring plan ensures that monitoring is performed for all components and that in these cases all the requirements of the JI guidelines and further guidance by the JISC regarding monitoring are met.

3. BASELINE SETTING

Baseline emission factor for Line 3 has been established on a line-specific basis. Campaign used for baseline measurements on the Line 3 has been carried out from 02/03/2007 through 14/07/2008. Nitric acid production during this campaign did not exceed the historic nitric acid production established as an average production during previous historic campaigns.

N₂O concentration and gas volume flow are monitored by monitoring system complying with requirements of the European Norm 14181.

Monitoring system provides separate readings for N₂O concentration and gas flow volume for every hour of operation as an average of the measured values for the previous 60 minutes.

Measurement results can be distorted before and after periods of downtime or malfunction of the monitoring system and can lead to mavericks. To eliminate such extremes and to ensure a conservative approach, the following statistical evaluation is applied to the complete data series of N₂O concentration as well as to the data series for gas volume flow. The statistical procedure is applied to data obtained after eliminating data measured for periods where the plant operated outside the permitted ranges:

- a) Calculate the sample mean (x)
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG))

The average mass of N₂O emissions per hour is estimated as product of the NCSG and VSG. The N₂O emissions per campaign are estimates product of N₂O emission per hour and the total number of complete hours of operation of the campaign using the following equation:

$$BE_{BC} = VSG_{BC} * NCSG_{BC} * 10^{-9} * OH_{BC} (tN_2O)$$

The line specific baseline emissions factor representing the average N₂O emissions per tonne of nitric acid over one full campaign is derived by dividing the total mass of N₂O emissions by the total output of 100% concentrated nitric acid during baseline campaign.

The overall uncertainty of the monitoring system has been calculated based on the 2008 QAL2 report in its sections 7.5 (also in table 10.5) where separate UNC values for N₂O concentration and tail gas flow are defined. The NA4 QAL2 test report does not contain calculation of total AMS UNC value, only separate UNC values for N₂O concentration and tail gas flow. Total AMS UNC is therefore calculated as $UNC = \sqrt{(2.88^2 + 1.83^2)}$. Total UNC is then 3.41%.

The N₂O emission factor per tonne of nitric acid produced in the baseline period (EFBL) has been then be reduced by the percentage error as follows:

$$EF_{BL} = (BE_{BC} / NAP_{BC}) (1 - UNC/100) (tN_2O/tHNO_3)$$

where:

Variable	Definition
EF_{BL}	Baseline N_2O emissions factor ($tN_2O/tHNO_3$)
BE_{BC}	Total N_2O emissions during the baseline campaign (tN_2O)
$NCSG_{BC}$	Mean concentration of N_2O in the stack gas during the baseline campaign (mgN_2O/m^3)
OH_{BC}	Operating hours of the baseline campaign (h)
VSG_{BC}	Mean gas volume flow rate at the stack in the baseline measurement period (m^3/h)
NAP_{BC}	Nitric acid production during the baseline campaign ($tHNO_3$)
UNC	Overall uncertainty of the monitoring system (%), calculated as the combined uncertainty of the applied monitoring equipment.

3.1 Measurement procedure for N_2O concentration and tail gas volume flow

3.1.1 Tail gas N_2O concentration

- the impulse line is the same as the NO_x outlet line
- the circuit is the same as for measuring NO_x outlet concentration, including up to the pressure reducing valve outlet.
- the gas for the N_2O analyzer is taken from here through a water discharge cooler. The analyzer is produced by Environement S.A., France and is based on non-dispersive infrared absorption principle; it is placed in the same cabinet as the NO_x analyzer. The N_2O concentration measurement range is between 0 – 2000 ppm.
- the outlet analyzer signal is of 4 – 20 mA, proportional to the value of the concentration. This signal is transmitted through an electric cable at the plant's central control panel. The electric cable is approx. 100 m long.
- the device that converts the 4 – 20 mA signal in nitrogen oxides concentration is a ISU – MMC- 24C digital indicator produced by Infostar Pascani. The device has 16 inlet circuits of 4 – 20 mA. The readings are digitally displayed and are recorded every 2 seconds. Data recorded into the "data logger" are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer's hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

3.1.2 Tail gas flow, temperature and pressure

- the measuring point is located on the expansion turbine outlet pipe towards the discharge nozzle; Pytot type sensor with multiple holes; operating conditions: absolute $p = 2.5$ bar, $t = 80^{\circ}\text{C}$

- pneumatic connection line (12 mm diameter and approx. 1 m long hoses) between the sensor and the electric switch box where the Dp cell is located; pneumatic connection line (6 mm diameter and approx. 2 m long hose) between the sensor and the electric switch box where the absolute pressure measuring cell is located

- measuring device: Dp differential transducer, produced by ABB, measuring range between 0 – 30 mbar; absolute pressure transducer produced by Endress&Hauser,

measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C ; analogue output signal 4 – 20 mA

- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA

- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.

- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

3.2 Permitted range of operating conditions of the nitric acid plant

Under certain circumstances, the operating conditions during the measurement period used to determine baseline N_2O emission factor may be outside the permitted range or limit corresponding to normal operating conditions. N_2O baseline data measured during hours where the operating conditions were outside the permitted range have been eliminated from the calculation of the baseline emissions factor.

Normal ranges for operating conditions have been determined for the following parameters:

- oxidation temperature;
- oxidation pressure;
- ammonia gas flow rate,
- air input flow rate.

The permitted range for these parameters has been established using the plant operation manual, as described in the PDD.

3.3 Composition of the ammonia oxidation catalyst

It is business-as-usual in Azomures to change composition of oxidation catalysts installed between campaigns, so the composition during historic and the baseline campaigns is varying.

Supplier of primary catalysts for plant NA4 between baseline campaign and fourth project campaign remained same as well as its composition. Use of this type of primary catalysts is the industry standard.

3.4 Historic Campaign Length

The average historic campaign length (CL_{normal}) defined as the average campaign length for the historic campaigns used to define operating condition (the previous 4 campaigns), has been used as a cap on the length of the baseline campaign.

3.5 Regulatory baseline emissions factor

There are no regulatory limits of N₂O whether defined as mass or concentration limits existent in Romania and there are no limits defined in the Azomures IPPC permit. Project thus uses baseline emission factor as measured during the baseline campaign.

4. PROJECT EMISSIONS

During the fourth project campaign on Line 3 the tail gas volume flow in the stack of the nitric acid plant as well as N₂O concentration have been measured on a continuous basis.

4.1.1 Estimation of campaign-specific project emissions factor

The monitoring system was installed using the guidance document EN 14181 and provides separate readings for N₂O concentration and gas flow volume for every hour of operation. Same statistical evaluation that was applied to the baseline data series has been applied to the project data series:

- a) Calculate the sample mean (\bar{x})
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values

$$PE_n = VSG * NCSG * 10^{-9} * OH \text{ (tN}_2\text{O)}$$

where:

Variable	Definition
VSG	Mean stack gas volume flow rate for the project campaign (m ³ /h)
NCSG	Mean concentration of N ₂ O in the stack gas for the project campaign (mgN ₂ O/m ³)
PE _n	Total N ₂ O emissions of the n th project campaign (tN ₂ O)
OH	Is the number of hours of operation in the specific monitoring period (h)

4.1.2 Derivation of a moving average emission factor

Because the project emission factor measured was lower than the moving average EF of the campaigns on this line so far, we have used the average EF for the calculation of the quantity of emission reductions generated during this campaign.

4.2 Minimum project emission factor

Because this campaign was fourth project campaign on Line 3 there has been no minimum average emission factor established yet for this campaign. This factor will be established after 10th project campaign.

4.3 Project Campaign Length

Project campaign production of nitric acid 30 571 tHNO₃ was lower than the nameplate capacity of the plant. Project campaign length was shorter than the historic campaign length and also shorter than the baseline campaign length and thus the baseline campaign length in terms of the N₂O concentration measurements has been shortened for calculation of the baseline emission factor and the emission reductions.

4.4 Leakage

No leakage calculation is required.

4.5 Emission reductions

The emission reductions for the project activity during this campaign have been determined by deducting the campaign-specific emission factor from the baseline emission factor and multiplying the result by the production output of 100% concentrated nitric acid over the campaign period and the GWP of N₂O:

$$ER = (EFBL - EFP) * NAP * GWPN_2O \text{ (tCO}_2\text{e)}$$

Where:

Variable	Definition
ER	Emission reductions of the project for the specific campaign (tCO ₂ e)
NAP	Nitric acid production for the project campaign (tHNO ₃). The maximum value of NAP shall not exceed the design capacity.
EFBL	Baseline emissions factor (tN ₂ O/tHNO ₃)
EFP	Emissions factor used to calculate the emissions from this particular campaign (i.e. the higher of EF _{ma,n} and EF _n)

5. MONITORING PLAN

5.1 Main air flow

- the measuring point is located on the compressor air discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 10 m long
- measuring device: Fischer Rosemount differential electronic transducer, having a measuring range between 0 – 45.24 mbar; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 30 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.2 Secondary air flow

- the measuring point is located on the air compressor discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 15 m long

- measuring device: Fischer Rosemount differential electronic transducer, having a measuring range between 0 – 500 mm H₂O; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 50 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.3 Casing protection air flow

- the measuring point is located on the air duct to the reactors casing, ramifications from the compressor discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 10 m long
- measuring device: FEPA Birlad differential electronic transducer, having a measuring range between 0 – 1500 mm H₂O; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 60 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.4 Reactor sieves temperature

- the measuring point is located on the oxidation reactor; sensor; PtRh-Pt thermocouple, operating conditions: $t = 800 - 1000^{\circ}\text{C}$
- electric signal transmission between the sensor and the transducer: PtRh-Pt correction cable, approx. 50 m long
- digital indicator measuring device; measuring range between $0 - 1000^{\circ}\text{C}$; analogue output signal $4 - 20 \text{ mA}$
- signal transmission: electric wires, approx. 6 m long, analogue signal $4 - 20 \text{ mA}$
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.5 Consumed liquid ammonia flow

- the measuring point is located on the ammonia evaporator inlet pipe; Coriolis type sensor; operating conditions: $p = 12 \text{ bar}$, $t = 8 - 10^{\circ}\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 90 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between $0 - 20 \text{ t/h}$; analogue output signal $4 - 20 \text{ mA}$
- signal transmission: electric wires, approx. 10 m long, analogue signal $4 - 20 \text{ mA}$
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.6 Flow of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; electromagnetic sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between 0 – 100 t/h; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.7 Temperature of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; Coriolis type sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between $-50 - 200^\circ\text{C}$; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this

database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.8 Density of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; Coriolis type sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between 1.2 – 1.4 kg/l; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.9 Tail gases flow, tail gases pressure, tail gases temperature

- the measuring point is located on the expansion turbine outlet pipe towards the discharge nozzle; Pytot type sensor with multiple holes; operating conditions: absolute $p = 2.5 \text{ bar}$, $t = 80^\circ\text{C}$
- pneumatic connection line (12 mm diameter and approx. 1 m long hoses) between the sensor and the electric switch box where the Dp cell is located; pneumatic connection line (6 mm diameter and approx. 2 m long hose) between the sensor and the electric switch box where the absolute pressure measuring cell is located
- measuring device: Dp differential transducer, produced by ABB, measuring range between 0 – 30 mbar; absolute pressure transducer produced by Endress&Hauser, measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA

- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.10 Oxidation reactor pressure

- the measuring point is located on the air compressor discharge pipe; sensor type: capsule for electronic transducer; operating conditions: absolute $p = 3.5$ bar, $t = 200^{\circ}\text{C}$
- pneumatic connection line between the sensor and the transducer; pneumatic connection line of 8 mm diameter and approx. 10 m long
- measuring device: Foxboro transducer, measuring range between 0 – 5 bar; absolute pressure transducer produced by Endress&Hauser, measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C ; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 50 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.11 N₂O concentration

- the impulse line is the same as the NOx outlet line
- the circuit is the same as for measuring NOx outlet concentration, including up to the pressure reducing valve outlet.
- the gas for the N₂O analyzer is taken from here through a water discharge cooler. The analyzer is produced by Environement S.A., France and is based on non-dispersive infrared

absorption principle; it is placed in the same cabinet as the NOx analyzer. The N2O concentration measurement range is between 0 – 2000 ppm.

- the outlet analyzer signal is of 4 – 20 mA, proportional to the value of the concentration. This signal is transmitted through an electric cable at the plant's central control panel. The electric cable is approx. 100 m long.
- the device that converts the 4 – 20 mA signal in nitrogen oxides concentration is a ISU – MMC- 24C digital indicator produced by Infostar Pascani. The device has 16 inlet circuits of 4 – 20 mA. The readings are digitally displayed and are recorded every 2 seconds. Data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer's hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

6. QAL 2 CALIBRATION ADJUSTMENTS

6.1 Applied principle

As required in the applicable norm EN14181: “The relation between the instrument readings of the recording measuring procedure and the quantity of the measuring objects has to be described by using a suitable convention method. The results have to be expressed by a regression analysis.”

QAL2 test providing regression lines and the combined uncertainty as further used in the model was performed in February 25 28, 2008 by company Airtec holding the ISO 17025 accreditation. During AST tests in August 3 – 6, 2009 and October 28, 2010 done by company SGS holding the ISO 17025 accreditation the NA4 measurements passed the test.

Measurement results derived from the analog signals (4 mA to 20 mA) provided the installed instruments have been compared to the comparative measurements.

Linearity check of the instruments characteristics is stated in the QAL2 Calibration Report issued by the laboratory. The valid ranges of linearity are determined by statistical analysis according to the guideline and the linearity assumptions are further used in the Calibration Report establishing linear regression lines.

The general formula of the regression line, established in the EN14181 and used in the Calibration Report is:

$$Y = a + bX$$

where:

X is the measured value of the instrument in mA
Y is the value of the parameter being objective of the measurement
a is a constant of the regression line
b is the slope of the regression line

After a comparative test the laboratory issued the old and new regression lines properties, namely “a” and “b” applying for all of the measured parameters that are subject to calibration as stated in the Calibration Report.

The QAL2 corrections are based on the fact that the actual analog current outputs (in mA) of the measurement instruments are relevant for both, the old and new regression lines:

$$X_o = X_n = X$$

where :

Xn: X new
Xo: X old

This allows us to derive a calibrating formula that gives us the corrected value of the measured physical parameters. The applied calibrating equation is:

$$Y_n = A_n + (B_n/B_o) * (Y_o - A_o)$$

In order to take into account the properties of the AMS and their implication to the QAL 2 implementation in the model, we will further introduce several remarks to the conversion and normalization of the data.

The units returned by the AMS in “Nm³/h” stand for normalized cubic meters of the gas volume at normal gas conditions (0° C, 1 atm.).

6.2 Stack gas volume flow

The measurement system captures and logs normalized stack volume flow in an integrated manner, calculating the final figure from the mA signal of the endpoints by itself, as opposing to storing just temperature and pressure and deriving the volume flow later. Therefore, the volume flow values can be used as input for QAL2 recalibration transformation without de-normalization and the need for temperature, pressure, and duct cross-section area. The normalized calibrated stack gas flow rates are further fed into the emission calculation model for processing as set out by the Approved Baseline and Monitoring Methodology AM_0034.

6.3 Nitrous oxide concentration in stack gas

The nitric acid concentration in the raw data set from the AMS is in ppm (parts per million). After QAL2 re-calibration, the values are converted to mgN₂O/Nm³ (mg N₂O per normalized cubic meter) to make it fit into the formulas set out in the methodology.

7. EMISSION REDUCTION CALCULATIONS

Table T 2 illustrates the establishment of historic campaign length based on 4 previous campaigns. Average production in campaigns preceding the baseline campaign was 286 940 tHNO₃ and time duration was on average 383 days. Table contains also information on suppliers of primary catalysts for Line 3 (4 burners). As shown in the table, it is usual practice in Azomures to use primary catalysts from two suppliers.

T 2 Historic campaigns

Line	AzoMures-3	Production	Start	End	Days	Production per day	Primary Catalyst	Composition
Historic Campaigns	1 t HNO ₃	-	-	-	-	n/a		0 N/A
	2 t HNO ₃	210 275	12 Oct 2001	27 Oct 2002	380	553	Engelhart-Cal	N/A *
	3 t HNO ₃	325 002	08 Nov 2002	13 Apr 2004	522	623	Engelhart-Cal	N/A *
	4 t HNO ₃	349 459	20 Apr 2004	02 Oct 2005	530	659	Engelhart-Cal	N/A *
	5 t HNO ₃	263 025	19 Oct 2005	16 Feb 2007	485	542	Johnson Matthey	N/A *
Average HNO₃ production		286 940			383	748	* Confidential, but available for verification	
Project Campaigns	BL t HNO ₃	215 669	02 Mar 2007	14 Jul 2008	500	432	Johnson Matthey	N/A *
	PL t HNO ₃	30 571	08 Oct 2012	19 Nov 2012	42	725	Johnson Matthey	N/A *

Table The project campaign production value of 30 571 tHNO₃ was lower than historic nitric acid production set at level of 286 940 tHNO₃.

T 3 and Chart C 1 define the length of the baseline campaign set according to the historic campaign length. Baseline campaign measurements was carried out from 02/03/2007 through 14/07/2008. During baseline campaign, a total of 215 669 tHNO₃ was produced, NCSG measurements are taken into account until the production of 30 097 tHNO₃ was reached.

The project campaign production value of 30 571 tHNO₃ was lower than historic nitric acid production set at level of 286 940 tHNO₃.

T 3 Baseline campaign length

AzoMures-3	Historic Campaigns End	Start of Baseline Measurement	End of Baseline Measurement NCSG	End of Baseline Measurement	End of Baseline Campaign
Dates	2007 Feb 16	2007 Mar 02	2007 Jul 09	2008 Jul 14	2008 Jul 15
Baseline Factor kgN ₂ O/tHNO ₃	-	-	9.40	9.40	9.40
Production tHNO ₃	-	-	30 097	215 669	-
Per Day Production tHNO ₃	748.4				
Baseline less Historic Production	(71 271.0)				
Baseline less Historic Days	(95.2)				

C 1 Baseline campaign length

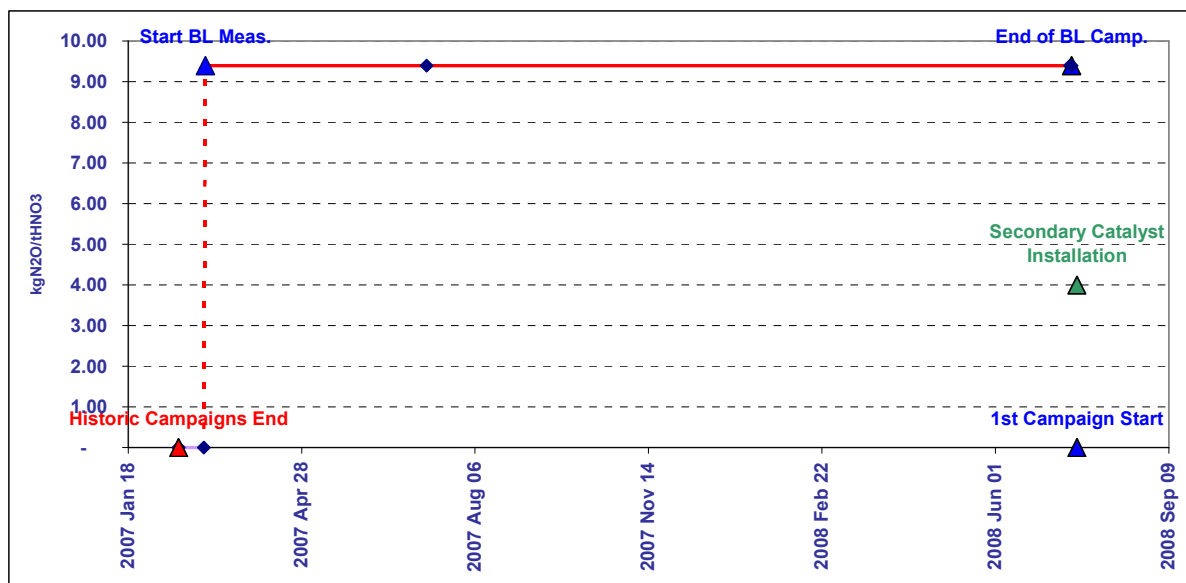


Table T 4 illustrates the calculation of the baseline emission factor on Line 3 using the method as defined in the CDM methodology AM0034 and in the PDD. Baseline measurement was carried out from 02/03/2007 through 14/07/2008.

Extreme values and data measured during hours when one or more of operating conditions were outside of the permitted range have been eliminated from the calculations. As a next step we have eliminated data beyond 95% confidence interval and calculated new mean values of N₂O concentration and stack gas volume flow using following method:

- Calculate the sample mean (x)
- Calculate the sample standard deviation (s)
- Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- Eliminate all data that lie outside the 95% confidence interval
- Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG))

Using the means values we have calculated the baseline emissions as set out in the PDD.

$$BE_{BC} = VSG_{BC} * NCSG_{BC} * 10^{-9} * OH_{BC} (tN_2O)$$

Operating hours defined as hours, when nitric acid production at least 0.1 tHNO₃ and oxidation temperature at least 640°C occurred. Calculated baseline N₂O emissions were 1,194 tN₂O.

$$EF_{BL} = (BE_{BC} / NAP_{BC}) (1 - UNC/100) (tN_2O/tHNO_3)$$

The UNC factor defined by the QAL2 report is 3.185%. As a result we have arrived to the baseline emission factor of 9.40 kgN₂O/tHNO₃.

Table T5 shows the calculation of the project emission factor on Line 3 during the project campaign. Project campaign started on 08/10/2012 and went through 19/11/2012.

We have eliminated extreme values and data beyond the 95% confidence interval as prescribed by the PDD.

- a) Calculate the sample mean (\bar{x})
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values

Using the mean values we have calculated total mass of N_2O emissions (PE_n) as follows:

$$PE_n = VSG * NCSG * 10^{-9} * OH (tN_2O)$$

Operating hours (OH) defined as hours, when nitric acid production at least 0.1 tHNO₃ and oxidation temperature at least 640°C occurred.

By dividing total mass of N_2O emissions by the nitric acid production (capped by nameplate capacity 725 tHNO₃/day) we have determined the project campaign specific emission factor at value of 1.95 kgN₂O/tHNO₃.

$$EF_n = PE_n / NAP_n (tN_2O/tHNO_3)$$

This emission factor has been used in further calculation of emission reductions. Neither moving average emission factor nor minimum emission factor was established, since it was the first project campaign.

T 4 Baseline emission factor

BASELINE EMISSION FACTOR									
Parameter	Operating Hours	Nitric Acid Production	N2O Concentration	Gas Volume Flow	Ammonia Flow Rate	Ammonia to Air Ratio	Oxidation Temperature	Oxidation Pressure	Code Unit
OH	NAP	NCSG	VSG	AFR	AIFR	OT	OP		
h	t/h	mg N2O/Nm3	Nm3/h	Nm3/h	%	°C	kPa		
Elimination of extreme values									
Lower limit	0	100	20 000	0	0	-	50	0	
Upper limit	60.00	5 000	200 000	18 000	20.00	1 200	1 000	1 000	
Raw Data Measured Range									
Count	8 624	7 388	6 482	11 915	11 174	11 989	11 431	11 431	
as % of Dataset	72%	62%	54%	99%	93%	100%	95%	95%	
Minimum	0.10	181	20 263	-	-	(31)	-	-	
Maximum	40.54	4 321	136 304	15 445	19.94	864	400	400	
Mean	29.19	4 260	95 572	7 882	8.53	623	104	104	
Standard Deviation	4.80	351	15 376	4 881	4.22	356	117	117	
Total	215 669								
N2O Emissions (VSG * NCSG * OH)									
Emission Factor	3 511	t N2O							
	15.76	kgN2O / tHNO3							
Permitted Range									
Minimum				8 000	0	800	0	0	
Maximum				12 500	11.50	860	260	260	
Data within the permitted range									
Count	8 291	982	6 924						
as % of Operating Hours	96%	11%	80%						
Minimum		824	-						
Maximum		4 321	415 934						
Mean		2 322	93 138						
Standard Deviation		1 470	21 931						
N2O Emissions (VSG * NCSG * OH)									
Emission Factor	1 865	t N2O							
	8.37	kgN2O / tHNO3							
Data within the confidence interval									
95% Confidence interval									
Lower bound		560	50 153						
Upper bound		5 203	136 122						
Count									
as % of Operating Hours		835	6 468						
Minimum		10%	75%						
Maximum		1 028	50 192						
Mean		4 321	135 386						
Standard Deviation		2 573	94 322						
		1 456	14 628						
N2O Emissions (VSG * NCSG * OH)									
Emission Factor (EF_BL)	2 093	t N2O							
	9.40	kgN2O / tHNO3							



T 5 Project emission factor

PROJECT EMISSION FACTOR									
Parameter	Operating Hours	Nitric Acid Production	N2O Concentration	Gas Volume Flow	Ammonia Flow Rate	Ammonia to Air Ratio	Oxidation Temperature	Oxidation Pressure	
Code Unit	OH h	NAP t/h	NCSG mg N2O/Nm3	VSG Nm3/h	AFR Nm3/h	AIFR %	OT °C	OP kPa	
Elimination of extreme values									
Lower limit		0	100	20 000	0	0	50	0	
Upper Limit		60.00	5 000	200 000	18 000	20.00	1 200	1 000	
Raw Data Measured Range									
Count	899	911	905	906	1 008	915	1 008	912	
as % of Dataset	89%	90%	90%	90%	100%	91%	100%	91%	
Minimum		0.61	102	27 782	35	0	(31)	0	
Maximum		36.89	680	117 773	12 233	12.49	839	258	
Mean		33.78	430	114 052	10 524	10.47	745	247	
Standard Deviation		3.67	34	4 830	3 559	1.10	255	23	
Total		30 774							
N2O Emissions (VSG * NCSG * OH)									
Emission Factor	44	t N2O							
	1.43	kgN2O / tHNO3							
Data within the confidence interval									
95% Confidence interval									
Lower bound				363	104 584				
Upper bound				498	123 519				
Count				878	895				
as % of Operating Hours				98%	100%				
Minimum				363	110 900				
Maximum				483	117 773				
Mean				432	114 418				
Standard Deviation				26	1 396				
N2O Emissions (VSG * NCSG * OH)									
Actual Project Emission Factor (EF_P Actual)	44	t N2O							
Abatement Ratio	1.45	kgN2O / tHNO3							
	84.6%								
Moving Average Emission Factor Correction									
	Actual Factors	Moving Average Rule							
1	1.45	1.45							
2	2.94	2.94							
3	1.98	2.12							
4	1.45	1.95							
Project Emission Factor (EF_P)									
Abatement Ratio	1.95	kgN2O / tHNO3							
	79.2%								

MONITORING REPORT

PROJECT: Project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA, company situated in Targu Mures, Romania

LINE: Line 4

MONITORING PERIOD:

FROM: 15/08/2012

TO: 19/11/2012

Prepared by:



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1. EXECUTIVE SUMMARY

This monitoring report determines baseline emission factor for the Line 4 of Azomures nitric acid plant and quantity of emission reduction generated during the fourth project campaign on the line.

Total quantity of emission reductions generated during the period from 15/08/2012 through 19/11/2012 on Line 4 is **133 550 ERUs**.

T 1 Emission reduction calculations

EMISSION REDUCTION		
Baseline Emission Factor	EF_BL	7.50 kgN ₂ O/tHNO ₃
Project Campaign Emission Factor	EF_P	1.51 kgN ₂ O/tHNO ₃
Nitric Acid Produced in the Baseline Campaign	NAP_BL	213 874 tHNO ₃
Nitric Acid Produced in the NCSG Baseline Campaign	NAP_BL_NCSG	78 517 tHNO ₃
Nitric Acid Produced in the Project Campaign	NAP_P	72 000 tHNO ₃
GWP	GWP	310 tCO ₂ e/tN ₂ O
Emission Reduction	ER	133 550 tCO₂e
<i>ER=(EF_BL-EF_P)*NAP_P*GWP/1000</i>		
Abatement Ratio	87.9%	

EMISSION REDUCTION PER YEAR			
Year	2010	2011	2012
Date From			15 Aug 2012
Date To			19 Nov 2012
Nitric Acid Production			72 000
Emission Reduction			133 550
<i>ER_YR = ER * NAP_P_YR / NAP_P</i>			

Baseline emission factor established for the Line 4 is 7.50 kgN₂O/tHNO₃. The baseline was carried out using overlapping technique. The first part of the baseline is the interval from 10/03/2008 to 10/08/2008, and it is completed by the second part from 06/04/2007 to 10/03/2008, thus adding up to a comparable campaign.

The secondary catalyst on Line 4 was installed on 11/08/2008. Project emission factor during the fourth project campaign, which started on 15/08/2012 and went through 19/11/2012, is 1.51 kgN₂O/tHNO₃.

During the project campaign 72 000 tonnes of nitric acid was produced.

2. DESCRIPTION OF THE PROJECT ACTIVITY

Purpose of the Project (the “Project”) is the reduction of nitrous oxide (N₂O) emissions from Joint Implementation project aimed at N₂O emissions reduction by installation of secondary catalyst inside ammonia oxidation reactors at 3 nitric acid production plants NA2, NA3 and NA4 of Azomures SA company, situated at Târgu Mures, Romania.

Azomures has installed and operates secondary N₂O reduction catalysts underneath the primary catalyst precious metal catching and catalytic gauzes package in the ammonium burners of all 3 nitric acid plants.

This monitoring report contains information on Line 4 emission reductions including information on baseline emission factor setting for the Line 4.

The separate treatment of the three nitric acid lines and overlapping of the monitoring periods are allowed by the clarification issued Joint Implementation Supervisory Committee: “CLARIFICATION REGARDING OVERLAPPING MONITORING PERIODS UNDER THE VERIFICATION PROCEDURE UNDER THE JOINT IMPLEMENTATION SUPERVISORY COMMITTEE”. The Project meets all the requirement set out by the clarification:

1. The Project is composed of clearly identifiable components for which emission reductions or enhancements of removals are calculated independently; and
2. Monitoring is performed independently for each of these components, i.e. the data/parameters monitored for one component are not dependent on/effect data/parameters (to be) monitored for another component; and
3. The monitoring plan ensures that monitoring is performed for all components and that in these cases all the requirements of the JI guidelines and further guidance by the JISC regarding monitoring are met.

3. BASELINE SETTING

Baseline emission factor for Line 4 has been established on a line-specific basis. Campaign used for baseline measurements on the Line 4 has been carried out using overlapping technique. The first part of the baseline is the interval from 10/03/2008 to 10/08/2008, and it is completed by the second part from 06/04/2007 to 10/03/2008, thus adding up to a comparable campaign. Nitric acid production during this campaign did not exceed the historic nitric acid production established as an average production during previous historic campaigns.

N₂O concentration and gas volume flow are monitored by monitoring system complying with requirements of the European Norm 14181.

Monitoring system provides separate readings for N₂O concentration and gas flow volume for every hour of operation as an average of the measured values for the previous 60 minutes.

Measurement results can be distorted before and after periods of downtime or malfunction of the monitoring system and can lead to mavericks. To eliminate such extremes and to ensure a conservative approach, the following statistical evaluation is applied to the complete data series of N₂O concentration as well as to the data series for gas volume flow. The statistical procedure is applied to data obtained after eliminating data measured for periods where the plant operated outside the permitted ranges:

- a) Calculate the sample mean (x)
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG))

The average mass of N₂O emissions per hour is estimated as product of the NCSG and VSG. The N₂O emissions per campaign are estimates product of N₂O emission per hour and the total number of complete hours of operation of the campaign using the following equation:

$$BE_{BC} = VSG_{BC} * NCSG_{BC} * 10^{-9} * OH_{BC} (tN_2O)$$

The line specific baseline emissions factor representing the average N₂O emissions per tonne of nitric acid over one full campaign is derived by dividing the total mass of N₂O emissions by the total output of 100% concentrated nitric acid during baseline campaign.

The overall uncertainty of the monitoring system has been calculated based on the 2008 QAL2 report in its sections 7.5 (also in table 10.5) where separate UNC values for N₂O concentration and tail gas flow are defined. The NA4 QAL2 test report does not contain calculation of total AMS UNC value, only separate UNC values for N₂O concentration and tail gas flow. Total AMS UNC is therefore calculated as $UNC = \sqrt{(2.88^2 + 1.83^2)}$. Total UNC is then 3.41%.

The N₂O emission factor per tonne of nitric acid produced in the baseline period (EF_{BL}) has been then be reduced by the percentage error as follows:

$$EF_{BL} = (BE_{BC} / NAP_{BC}) (1 - UNC/100) (tN_2O/tHNO_3)$$

where:

Variable	Definition
EF _{BL}	Baseline N ₂ O emissions factor (tN ₂ O/tHNO ₃)
BE _{BC}	Total N ₂ O emissions during the baseline campaign (tN ₂ O)
NCSG _{BC}	Mean concentration of N ₂ O in the stack gas during the baseline campaign (mgN ₂ O/m ³)
OH _{BC}	Operating hours of the baseline campaign (h)
VSG _{BC}	Mean gas volume flow rate at the stack in the baseline measurement period (m ³ /h)
NAP _{BC}	Nitric acid production during the baseline campaign (tHNO ₃)
UNC	Overall uncertainty of the monitoring system (%), calculated as the combined uncertainty of the applied monitoring equipment.

3.1 Measurement procedure for N₂O concentration and tail gas volume flow

3.1.1 Tail gas N₂O concentration

- the impulse line is the same as the NO_x outlet line
- the circuit is the same as for measuring NO_x outlet concentration, including up to the pressure reducing valve outlet.
- the gas for the N₂O analyzer is taken from here through a water discharge cooler. The analyzer is produced by Environement S.A., France and is based on non-dispersive infrared absorption principle; it is placed in the same cabinet as the NO_x analyzer. The N₂O concentration measurement range is between 0 – 2000 ppm.
- the outlet analyzer signal is of 4 – 20 mA, proportional to the value of the concentration. This signal is transmitted through an electric cable at the plant's central control panel. The electric cable is approx. 100 m long.
- the device that converts the 4 – 20 mA signal in nitrogen oxides concentration is a ISU – MMC- 24C digital indicator produced by Infostar Pascani. The device has 16 inlet circuits of 4 – 20 mA. The readings are digitally displayed and are recorded every 2 seconds. Data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer's hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

3.1.2 Tail gas flow, temperature and pressure

- the measuring point is located on the expansion turbine outlet pipe towards the discharge nozzle; Pytot type sensor with multiple holes; operating conditions: absolute $p = 2.5$ bar, $t = 80^{\circ}\text{C}$

- pneumatic connection line (12 mm diameter and approx. 1 m long hoses) between the sensor and the electric switch box where the Dp cell is located; pneumatic connection line (6 mm diameter and approx. 2 m long hose) between the sensor and the electric switch box where the absolute pressure measuring cell is located

- measuring device: Dp differential transducer, produced by ABB, measuring range between 0 – 30 mbar; absolute pressure transducer produced by Endress&Hauser,

measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C ; analogue output signal 4 – 20 mA

- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA

- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.

- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

3.2 Permitted range of operating conditions of the nitric acid plant

Under certain circumstances, the operating conditions during the measurement period used to determine baseline N_2O emission factor may be outside the permitted range or limit corresponding to normal operating conditions. N_2O baseline data measured during hours where the operating conditions were outside the permitted range have been eliminated from the calculation of the baseline emissions factor.

Normal ranges for operating conditions have been determined for the following parameters:

- oxidation temperature;
- oxidation pressure;
- ammonia gas flow rate,
- air input flow rate.

The permitted range for these parameters has been established using the plant operation manual, as described in the PDD.

3.3 Composition of the ammonia oxidation catalyst

It is business-as-usual in Azomures to change composition of oxidation catalysts installed between campaigns, so the composition during historic and the baseline campaigns is varying.

Supplier of primary catalysts for plant NA4 between baseline campaign and fourth project campaign remained same as well as its composition. Use of this type of primary catalysts is the industry standard.

3.4 Historic Campaign Length

The average historic campaign length (CL_{normal}) defined as the average campaign length for the historic campaigns used to define operating condition (the previous 4 campaigns), has been used as a cap on the length of the baseline campaign.

3.5 Regulatory baseline emissions factor

There are no regulatory limits of N₂O whether defined as mass or concentration limits existent in Romania and there are no limits defined in the Azomures IPPC permit. Project thus uses baseline emission factor as measured during the baseline campaign.

4. PROJECT EMISSIONS

During the fourth project campaign on Line 4 the tail gas volume flow in the stack of the nitric acid plant as well as N₂O concentration have been measured on a continuous basis.

4.1.1 Estimation of campaign-specific project emissions factor

The monitoring system was installed using the guidance document EN 14181 and provides separate readings for N₂O concentration and gas flow volume for every hour of operation. Same statistical evaluation that was applied to the baseline data series has been applied to the project data series:

- a) Calculate the sample mean (\bar{x})
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values

$$PE_n = VSG * NCSG * 10^{-9} * OH \text{ (tN}_2\text{O)}$$

where:

Variable	Definition
VSG	Mean stack gas volume flow rate for the project campaign (m ³ /h)
NCSG	Mean concentration of N ₂ O in the stack gas for the project campaign (mgN ₂ O/m ³)
PE _n	Total N ₂ O emissions of the n th project campaign (tN ₂ O)
OH	Is the number of hours of operation in the specific monitoring period (h)

4.1.2 Derivation of a moving average emission factor

Because the project emission factor measured was lower than the moving average EF of the campaigns on this line so far, we have used the average EF for the calculation of the quantity of emission reductions generated during this campaign.

4.2 Minimum project emission factor

Because this campaign was fourth project campaign on Line 4 there has been no minimum average emission factor established yet for this campaign. This factor will be established after 10th project campaign.

4.3 Project Campaign Length

Project campaign production of nitric acid 78 538 tHNO₃ was lower than the nameplate capacity of the plant. Project campaign length was shorter than the historic campaign length and also shorter than the baseline campaign length and thus the baseline campaign length in terms of the N₂O concentration measurements has been shortened for calculation of the baseline emission factor and the emission reductions.

4.4 Leakage

No leakage calculation is required.

4.5 Emission reductions

The emission reductions for the project activity during this campaign have been determined by deducting the campaign-specific emission factor from the baseline emission factor and multiplying the result by the production output of 100% concentrated nitric acid over the campaign period and the GWP of N₂O:

$$ER = (EFBL - EFP) * NAP * GWPN_2O \text{ (tCO}_2\text{e)}$$

Where:

Variable	Definition
ER	Emission reductions of the project for the specific campaign (tCO ₂ e)
NAP	Nitric acid production for the project campaign (tHNO ₃). The maximum value of NAP shall not exceed the design capacity.
EFBL	Baseline emissions factor (tN ₂ O/tHNO ₃)
EFP	Emissions factor used to calculate the emissions from this particular campaign (i.e. the higher of EF _{ma,n} and EF _n)

5. MONITORING PLAN

5.1 Main air flow

- the measuring point is located on the compressor air discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 10 m long
- measuring device: Fischer Roesmount differential electronic transducer, having a measuring range between 0 – 45.24 mbar; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 30 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.2 Secondary air flow

- the measuring point is located on the air compressor discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 15 m long

- measuring device: Fischer Roesmount differential electronic transducer, having a measuring range between 0 – 500 mm H₂O; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 50 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.3 Casing protection air flow

- the measuring point is located on the air duct to the reactors casing, ramifications from the compressor discharge pipe
- diaphragm type sensor with ring-like chambers
- operating conditions: $p = 2.5 - 3$ bars, $t = 150^{\circ}\text{C}$
- pneumatic signal transmission between the sensor and the transducer through 2 impulse pipes, approx. 10 m long
- measuring device: FEPA Birlad differential electronic transducer, having a measuring range between 0 – 1500 mm H₂O; output signal: analogue 4 – 20 mA
- signal transmission: electric wires, approx. 60 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.4 Reactor sieves temperature

- the measuring point is located on the oxidation reactor; sensor; PtRh-Pt thermocouple, operating conditions: $t = 800 - 1000^{\circ}\text{C}$
- electric signal transmission between the sensor and the transducer: PtRh-Pt correction cable, approx. 50 m long
- digital indicator measuring device; measuring range between $0 - 1000^{\circ}\text{C}$; analogue output signal $4 - 20 \text{ mA}$
- signal transmission: electric wires, approx. 6 m long, analogue signal $4 - 20 \text{ mA}$
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.5 Consumed liquid ammonia flow

- the measuring point is located on the ammonia evaporator inlet pipe; Coriolis type sensor; operating conditions: $p = 12 \text{ bar}$, $t = 8 - 10^{\circ}\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 90 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between $0 - 20 \text{ t/h}$; analogue output signal $4 - 20 \text{ mA}$
- signal transmission: electric wires, approx. 10 m long, analogue signal $4 - 20 \text{ mA}$
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.6 Flow of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; electromagnetic sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between 0 – 100 t/h; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.7 Temperature of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; Coriolis type sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between $-50 - 200^\circ\text{C}$; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this

database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.8 Density of produced nitric acid

- the measuring point is located on the column 4 outlet pipe towards the nitric acid storehouse; Coriolis type sensor; operating conditions: $p = 2.5 \text{ bar}$, $t = 40^\circ\text{C}$
- electric signal transmission between the sensor and the transducer: 2-wire cable, approx. 100 m long
- measuring device: DZL363 flowmeter adapter produced by Endress&Hauser; measuring range between 1.2 – 1.4 kg/l; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.9 Tail gases flow, tail gases pressure, tail gases temperature

- the measuring point is located on the expansion turbine outlet pipe towards the discharge nozzle; Pytot type sensor with multiple holes; operating conditions: absolute $p = 2.5 \text{ bar}$, $t = 80^\circ\text{C}$
- pneumatic connection line (12 mm diameter and approx. 1 m long hoses) between the sensor and the electric switch box where the Dp cell is located; pneumatic connection line (6 mm diameter and approx. 2 m long hose) between the sensor and the electric switch box where the absolute pressure measuring cell is located
- measuring device: Dp differential transducer, produced by ABB, measuring range between 0 – 30 mbar; absolute pressure transducer produced by Endress&Hauser, measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 5 m long, analogue signal 4 – 20 mA

- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.10 Oxidation reactor pressure

- the measuring point is located on the air compressor discharge pipe; sensor type: capsule for electronic transducer; operating conditions: absolute $p = 3.5$ bar, $t = 200^{\circ}\text{C}$
- pneumatic connection line between the sensor and the transducer; pneumatic connection line of 8 mm diameter and approx. 10 m long
- measuring device: Foxboro transducer, measuring range between 0 – 5 bar; absolute pressure transducer produced by Endress&Hauser, measuring range between 0 – 0.3 bar; Pt100 thermal resistance with built-in adapter, measuring range between 0 - 200°C ; analogue output signal 4 – 20 mA
- signal transmission: electric wires, approx. 50 m long, analogue signal 4 – 20 mA
- signal conversion device: ISU 24M digital indicator; placed inside the control panel; converts the analogue signal into digital signal; recording period: 2 seconds.
- data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer’s hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

5.11 N₂O concentration

- the impulse line is the same as the NOx outlet line
- the circuit is the same as for measuring NOx outlet concentration, including up to the pressure reducing valve outlet.
- the gas for the N₂O analyzer is taken from here through a water discharge cooler. The analyzer is produced by Environement S.A., France and is based on non-dispersive infrared

absorption principle; it is placed in the same cabinet as the NOx analyzer. The N2O concentration measurement range is between 0 – 2000 ppm.

- the outlet analyzer signal is of 4 – 20 mA, proportional to the value of the concentration. This signal is transmitted through an electric cable at the plant's central control panel. The electric cable is approx. 100 m long.
- the device that converts the 4 – 20 mA signal in nitrogen oxides concentration is a ISU – MMC- 24C digital indicator produced by Infostar Pascani. The device has 16 inlet circuits of 4 – 20 mA. The readings are digitally displayed and are recorded every 2 seconds. Data recorded into the “data logger” are transmitted through an optic fiber network to a computer designated particularly for this type of monitoring. This computer is located in the Instrumentation Plant. Data are stored in a database on the computer's hard disk. From this database data are afterwards processed in order to obtain all data necessary for the project. The entire database is periodically saved on graphic and magnetic support as an Excel file.

6. QAL 2 CALIBRATION ADJUSTMENTS

6.1 Applied principle

As required in the applicable norm EN14181: “The relation between the instrument readings of the recording measuring procedure and the quantity of the measuring objects has to be described by using a suitable convention method. The results have to be expressed by a regression analysis.”

QAL2 test providing regression lines and the combined uncertainty as further used in the model was performed in February 25 28, 2008 by company Airtec holding the ISO 17025 accreditation. During AST tests in August 3 – 6, 2009 and October 28, 2010 done by company SGS holding the ISO 17025 accreditation the NA4 measurements passed the test.

Measurement results derived from the analog signals (4 mA to 20 mA) provided the installed instruments have been compared to the comparative measurements.

Linearity check of the instruments characteristics is stated in the QAL2 Calibration Report issued by the laboratory. The valid ranges of linearity are determined by statistical analysis according to the guideline and the linearity assumptions are further used in the Calibration Report establishing linear regression lines.

The general formula of the regression line, established in the EN14181 and used in the Calibration Report is:

$$Y = a + bX$$

where:

X is the measured value of the instrument in mA
Y is the value of the parameter being objective of the measurement
a is a constant of the regression line
b is the slope of the regression line

After a comparative test the laboratory issued the old and new regression lines properties, namely “a” and “b” applying for all of the measured parameters that are subject to calibration as stated in the Calibration Report.

The QAL2 corrections are based on the fact that the actual analog current outputs (in mA) of the measurement instruments are relevant for both, the old and new regression lines:

$$X_o = X_n = X$$

where :

Xn: X new
Xo: X old

This allows us to derive a calibrating formula that gives us the corrected value of the measured physical parameters. The applied calibrating equation is:

$$Y_n = A_n + (B_n/B_o) * (Y_o - A_o)$$

In order to take into account the properties of the AMS and their implication to the QAL 2 implementation in the model, we will further introduce several remarks to the conversion and normalization of the data.

The units returned by the AMS in “Nm³/h” stand for normalized cubic meters of the gas volume at normal gas conditions (0° C, 1 atm.).

6.2 Stack gas volume flow

The measurement system captures and logs normalized stack volume flow in an integrated manner, calculating the final figure from the mA signal of the endpoints by itself, as opposing to storing just temperature and pressure and deriving the volume flow later. Therefore, the volume flow values can be used as input for QAL2 recalibration transformation without de-normalization and the need for temperature, pressure, and duct cross-section area. The normalized calibrated stack gas flow rates are further fed into the emission calculation model for processing as set out by the Approved Baseline and Monitoring Methodology AM_0034.

6.3 Nitrous oxide concentration in stack gas

The nitric acid concentration in the raw data set from the AMS is in ppm (parts per million). After QAL2 re-calibration, the values are converted to mgN₂O/Nm³ (mg N₂O per normalized cubic meter) to make it fit into the formulas set out in the methodology.

7. EMISSION REDUCTION CALCULATIONS

Table T 2 illustrates the establishment of historic campaign length based on 4 previous campaigns. Average production in campaigns preceding the baseline campaign was 275 871 tHNO₃ and time duration was on average 408 days. Table contains also information on suppliers of primary catalysts for Line 4 (4 burners). As shown in the table, it is usual practice in Azomures to use primary catalysts from two suppliers.

T 2 Historic campaigns

Line	AzoMures-4	Production	Start	End	Days	Production per day	Primary Catalyst	Composition
Historic Campaigns	1 t HNO ₃	-	-	-	-	n/a	N/A	N/A
	2 t HNO ₃	237 767	08 Dec 2000	16 Apr 2002	494	481	Engelhart-Cal	N/A *
	3 t HNO ₃	271 545	21 May 2002	20 Nov 2003	548	496	Engelhart-Cal	N/A *
	4 t HNO ₃	308 263	27 Nov 2003	06 Feb 2005	437	705	Engelhart-Cal	N/A *
	5 t HNO ₃	285 908	23 Feb 2005	05 Sep 2006	559	511	Heraeus	N/A *
Average HNO₃ production		t HNO₃	275 871		408	677	* Confidential, but available for verification	
Project Campaigns	BL t HNO ₃	213 874	06 Apr 2007	10 Aug 2008	492	435	Heraeus	N/A *
	PL t HNO ₃	72 000	15 Aug 2012	19 Nov 2012	96	750	Heraeus	N/A *

Table The project campaign production value of 78 538 tHNO₃ was lower than historic nitric acid production set at level of 275 871 tHNO₃.

T 3 and Chart C 1 define the length of the baseline campaign set according to the historic campaign length. Baseline campaign measurements was carried out using overlapping technique. The first part of the baseline is the interval from 10/03/2008 to 10/08/2008, and it is completed by the second part from 06/04/2007 to 10/03/2008, thus adding up to a comparable campaign. During baseline campaign, a total of 213 874 tHNO₃ was produced, NCSG measurements are taken into account until the production of 78 517 tHNO₃ was reached.

The project campaign production value of 78 538 tHNO₃ was lower than historic nitric acid production set at level of 275 871 tHNO₃.

T 3 Baseline campaign length

AzoMures-4	Historic Campaigns End	Start of Baseline Measurement	End of Baseline Measurement NCSG	End of Baseline Measurement	End of Baseline Campaign
Dates	2006 Sep 05	2007 Apr 06	2008 Jul 08	2008 Aug 10	2008 Aug 11
Baseline Factor kgN ₂ O/tHNO ₃	-	-	7.50	7.50	7.50
Production tHNO ₃	-	-	78 517	213 874	-
Per Day Production tHNO ₃	676.8				
Baseline less Historic Production	(61 996.8)				
Baseline less Historic Days	(91.6)				

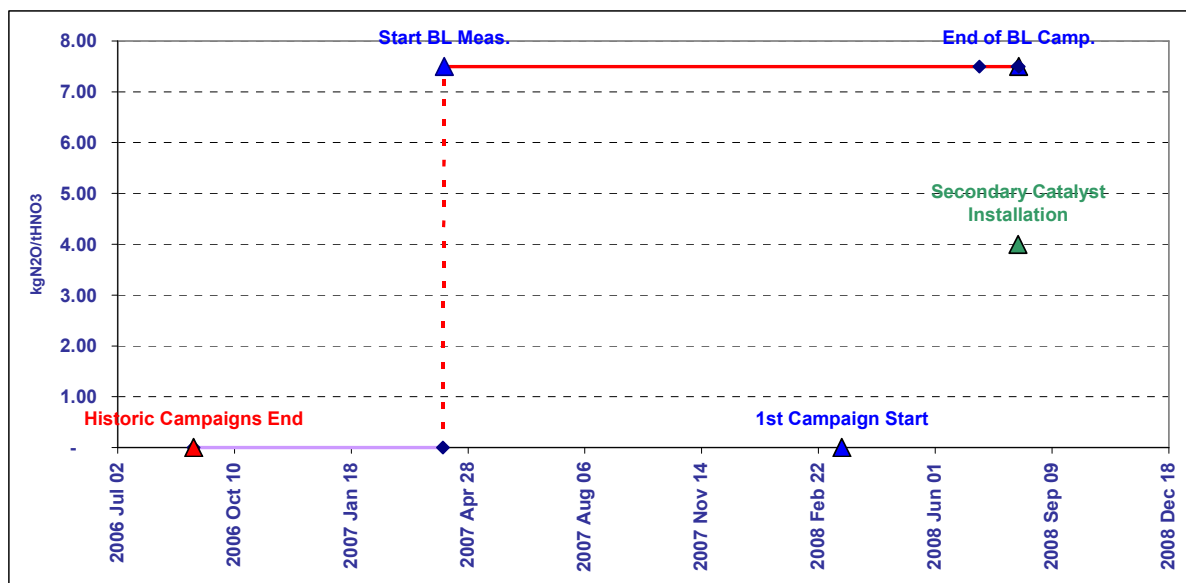
C 1 Baseline campaign length


Table T 4 illustrates the calculation of the baseline emission factor on Line 4 using the method as defined in the CDM methodology AM0034 and in the PDD. Baseline measurement was carried out using overlapping technique. The first part of the baseline is the interval from 10/03/2008 to 10/08/2008, and it is completed by the second part from 06/04/2007 to 10/03/2008, thus adding up to a comparable campaign.

Extreme values and data measured during hours when one or more of operating conditions were outside of the permitted range have been eliminated from the calculations. As a next step we have eliminated data beyond 95% confidence interval and calculated new mean values of N₂O concentration and stack gas volume flow using following method:

- a) Calculate the sample mean (x)
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG))

Using the means values we have calculated the baseline emissions as set out in the PDD.

$$BE_{BC} = VSG_{BC} * NCSG_{BC} * 10^{-9} * OH_{BC} (tN_2O)$$

Operating hours defined as hours, when nitric acid production at least 0.1 tHNO₃ and oxidation temperature at least 640°C occurred. Calculated baseline N₂O emissions were 1,194 tN₂O.

$$EF_{BL} = (BE_{BC} / NAP_{BC}) (1 - UNC/100) (tN_2O/tHNO_3)$$

The UNC factor defined by the QAL2 report is 3.412%. As a result we have arrived to the baseline emission factor of 7.50 kgN₂O/tHNO₃.

Table T5 shows the calculation of the project emission factor on Line 4 during the project campaign. Project campaign started on 15/08/2012 and went through 19/11/2012.

We have eliminated extreme values and data beyond the 95% confidence interval as prescribed by the PDD.

- a) Calculate the sample mean (\bar{x})
- b) Calculate the sample standard deviation (s)
- c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation)
- d) Eliminate all data that lie outside the 95% confidence interval
- e) Calculate the new sample mean from the remaining values

Using the mean values we have calculated total mass of N_2O emissions (PE_n) as follows:

$$PE_n = VSG * NCSG * 10^{-9} * OH \text{ (tN}_2\text{O)}$$

Operating hours (OH) defined as hours, when nitric acid production at least 0.1 tHNO₃ and oxidation temperature at least 640°C occurred.

By dividing total mass of N_2O emissions by the nitric acid production (capped by nameplate capacity 725 tHNO₃/day) we have determined the project campaign specific emission factor at value of 1.51 kgN₂O/tHNO₃.

$$EF_n = PE_n / NAP_n \text{ (tN}_2\text{O/tHNO}_3\text{)}$$

This emission factor has been used in further calculation of emission reductions. Neither moving average emission factor nor minimum emission factor was established, since it was the first project campaign.

T 4 Baseline emission factor

BASELINE EMISSION FACTOR									
Parameter	Operating Hours	Nitric Acid Production	N2O Concentration	Gas Volume Flow	Ammonia Flow Rate	Ammonia to Air Ratio	Oxidation Temperature	Oxidation Pressure	
Code Unit	OH h	NAP t/h	NCSG mg N2O/Nm3	VSG Nm3/h	AFR Nm3/h	AIFR %	OT °C	OP kPa	
Elimination of extreme values									
Lower limit		0	100	20 000	0	0	50	0	
Upper limit		60.00	5 000	200 000	18 000	20.00	1 200	1 000	
Raw Data Measured Range									
Count	8 186	7 063	2 473	7 986	11 803	10 639	11 809	10 866	
as % of Dataset	69%	60%	21%	68%	100%	90%	100%	92%	
Minimum	0.19	0.19	108	22 057	-	-	(25)	-	
Maximum	51.11	51.11	4 071	132 738	14 347	19.98	864	449	
Mean	30.28	30.28	2 101	94 338	8 396	9.20	628	149	
Standard Deviation	5.57	5.57	402	20 732	4 887	3.36	338	143	
Total		213 874							
N2O Emissions (VSG * NCSG * OH)									
Emission Factor	1 622 tN2O	7.33 kgN2O / tHNO3							
Permitted Range									
Minimum					8 000	0	800	180	
Maximum					13 800	11.50	860	300	
Data within the permitted range									
Count	4 682		2 272	4 682					
as % of Operating Hours	57%		28%	57%					
Minimum			248	64 742					
Maximum			4 071	689 625					
Mean			2 110	98 624					
Standard Deviation			382	26 454					
N2O Emissions (VSG * NCSG * OH)									
Emission Factor	1 703 tN2O	7.69 kgN2O / tHNO3							
Data within the confidence interval									
95% Confidence Interval									
Lower bound			1 361	46 774					
Upper bound			2 858	150 474					
Count	2 208		2 208	4 650					
as % of Operating Hours	27%		27%	57%					
Minimum			1 381	64 742					
Maximum			2 848	150 376					
Mean			2 086	97 244					
Standard Deviation			260	12 186					
N2O Emissions (VSG * NCSG * OH)									
Emission Factor (EF_BL)	1 660 tN2O	7.50 kgN2O / tHNO3							



T 5 Project emission factor

PROJECT EMISSION FACTOR										
Parameter	Operating Hours	Nitric Acid Production	N2O Concentration	Gas Volume Flow	Ammonia Flow Rate	Ammonia to Air Ratio	Oxidation Temperature	Oxidation Pressure		
Code Unit	OH h	NAP t/h	NCSG mg N2O/Nm3	VSG Nm3/h	AFR Nm3/h	AIFR %	OT °C	OP kPa		
Elimination of extreme values										
Lower limit	0	60.00	5.000	20.000	0	0	-	50	0	
Upper Limit				200.000	18.000	20.00	1.200	1.000		
Raw Data Measured Range										
Count	1 944	1 985	1 940	1 964	2 294	2 164	2 304	2 048		
as % of Dataset	84%	86%	84%	85%	100%	94%	100%	89%		
Minimum		0.27	105	23 969	-	-	(31)	-		
Maximum		54.93	663	131 557	14 675	19.06	765	288		
Mean		39.57	301	122 116	10 621	9.67	565	257		
Standard Deviation		5.38	66	7 746	4 471	2.54	318	56		
Total		78 538								
N2O Emissions (VSG * NCSG * OH)										
Emission Factor	72 t N2O									
	0.91 kgN2O / tHNO3									
Data within the confidence interval										
95% Confidence interval										
Lower bound				172	106 934					
Upper bound				431	137 298					
Count				1 879	1 923					
as % of Operating Hours				97%	99%					
Minimum				173	109 048					
Maximum				431	131 557					
Mean				299	122 779					
Standard Deviation				59	4 554					
N2O Emissions (VSG * NCSG * OH)										
Actual Project Emission Factor (EF_PAActual)	71 t N2O									
Abatement Ratio	0.91 kgN2O / tHNO3									
	87.9%									
Moving Average Emission Factor Correction										
	Actual Factors	Moving Average Rule								
1	1.48	1.48								
2	2.22	2.22								
3	1.45	1.72								
4	0.91	1.51								
Project Emission Factor (EF_P)										
Abatement Ratio	1.51 kgN2O / tHNO3									
	79.8%									